1.1

1.1 The force, F, of the wind blowing against a building is given by $F = C_D \rho V^2 A/2$, where V is the wind speed, ρ the density of the air, A the cross-sectional area of the building, and C_D is a constant termed the drag coefficient. Determine the dimensions of the drag coefficient.

$$F = C_D \rho V^2 A/2$$

or

$$C_D = 2F/\rho V^2 A \text{, where } F \doteq MLT^{-2}$$

$$\rho \doteq ML^{-3}$$

$$V \doteq LT^{-1}$$

$$A \doteq L^2$$

Thus,

$$C_D \doteq (MLT^{-2})/[(ML^{-3})(LT^{-1})^2(L^2)] = M^0 L^0 T^0$$

Hence, C_D is dimensionless.

4 h:

1.2

1.2 Determine the dimensions, in both the *FLT* system and the *MLT* system, for (**a**) the product of mass times velocity, (**b**) the product of force times volume, and (**c**) kinetic energy divided by area.

(a) $\text{mass} \times \text{velocity} \doteq (M)(LT^{-1}) \doteq \underline{\underline{MLT^{-1}}}$

Since $F \doteq MLT^{-2}$

$\text{mass} \times \text{velocity} \doteq (FL^{-1}T^{2})(LT^{-1}) \doteq \underline{\underline{FT}}$

(b) $\text{force} \times \text{volume} \doteq \underline{\underline{FL^3}}$

$\doteq (MLT^{-2})(L^3) \doteq \underline{\underline{ML^4T^{-2}}}$

(c) $\dfrac{\text{kinetic energy}}{\text{area}} \doteq \dfrac{FL}{L^2} \doteq \underline{\underline{FL^{-1}}}$

$\doteq \dfrac{(MLT^{-2})L}{L^2} \doteq \underline{\underline{MT^{-2}}}$

1.3

1.3 Verify the dimensions, in both the *FLT* and *MLT* systems, of the following quantities which appear in Table 1.1: **(a)** volume, **(b)** acceleration, **(c)** mass, **(d)** moment of inertia (area), and **(e)** work.

(a) volume $\doteq \underline{\underline{L^3}}$

(b) acceleration = time rate of change of velocity

$$\doteq \frac{LT^{-1}}{T} \doteq \underline{\underline{LT^{-2}}}$$

(c) mass $\doteq \underline{\underline{M}}$

or with $F \doteq MLT^{-2}$

mass $\doteq \underline{\underline{FL^{-1}T^2}}$

(d) moment of inertia (area) = second moment of area

$$\doteq (L^2)(L^2) \doteq \underline{\underline{L^4}}$$

(e) work = force × distance

$$\doteq \underline{\underline{FL}}$$

or with $F \doteq MLT^{-2}$

work $\doteq \underline{\underline{ML^2T^{-2}}}$

1.4

1.4 Determine the dimensions, in both the *FLT* system and the *MLT* system, for **(a)** the product of force times acceleration, **(b)** the product of force times velocity divided by area, and **(c)** momentum divided by volume.

(a) $\text{force} \times \text{acceleration} \doteq (F)(LT^{-2}) \doteq \underline{\underline{FLT^{-2}}}$

Since $F \doteq MLT^{-2}$,

$\text{force} \times \text{acceleration} \doteq (MLT^{-2})(LT^{-2}) \doteq \underline{\underline{ML^2T^{-4}}}$

(b) $$\frac{\text{force} \times \text{velocity}}{\text{area}} \doteq \frac{(F)(LT^{-1})}{L^2} \doteq \underline{\underline{FL^{-1}T^{-1}}}$$

$$\doteq \frac{(MLT^{-2})(LT^{-1})}{L^2} \doteq \underline{\underline{MT^{-3}}}$$

(c) $$\frac{\text{momentum}}{\text{volume}} = \frac{\text{mass} \times \text{velocity}}{\text{volume}}$$

$$\doteq \frac{(FT^2L^{-1})(LT^{-1})}{L^3} \doteq \underline{\underline{FL^{-3}T}}$$

$$\doteq \frac{(M)(LT^{-1})}{L^3} \doteq \underline{\underline{ML^{-2}T^{-1}}}$$

1.5

1.5 Verify the dimensions, in both the *FLT* and *MLT* systems, of the following quantities which appear in Table 1.1: **(a)** angular velocity, **(b)** energy, **(c)** moment of inertia (area), **(d)** power, and **(e)** pressure.

(a) angular velocity $= \dfrac{\text{angular displacement}}{\text{time}} \doteq \underline{\underline{T^{-1}}}$

(b) energy ~ capacity of body to do work

Since work = force × distance,

$$\text{energy} \doteq \underline{\underline{FL}}$$

or with $F \doteq MLT^{-2}$

$$\text{energy} \doteq (MLT^{-2})(L) \doteq \underline{\underline{ML^2T^{-2}}}$$

(c) moment of inertia (area) = second moment of area

$$\doteq (L^2)(L^2) \doteq \underline{\underline{L^4}}$$

(d) power = rate of doing work $\doteq \dfrac{FL}{T} \doteq \underline{\underline{FLT^{-1}}}$

$$\doteq (MLT^{-2})(L)(T^{-1}) \doteq \underline{\underline{ML^2T^{-3}}}$$

(e) pressure $= \dfrac{\text{force}}{\text{area}} \doteq \dfrac{F}{L^2} \doteq \underline{\underline{FL^{-2}}}$

$$\doteq (MLT^{-2})(L^{-2}) \doteq \underline{\underline{ML^{-1}T^{-2}}}$$

1.6

1.6 Verify the dimensions, in both the *FLT* system and the *MLT* system, of the following quantities which appear in Table 1.1: **(a)** frequency, **(b)** stress, **(c)** strain, **(d)** torque, and **(e)** work.

(a) $\text{frequency} = \dfrac{\text{cycles}}{\text{time}} \doteq \underline{\underline{T^{-1}}}$

(b) $\text{stress} = \dfrac{\text{force}}{\text{area}} \doteq \dfrac{F}{L^2} \doteq \underline{\underline{FL^{-2}}}$

Since $F \doteq MLT^{-2}$,

$$\text{stress} \doteq \frac{MLT^{-2}}{L^2} \doteq \underline{\underline{ML^{-1}T^{-2}}}$$

(c) $\text{strain} = \dfrac{\text{change in length}}{\text{length}} \doteq \dfrac{L}{L} \doteq \underline{\underline{L^0}}$ (dimensionless)

(d) $\text{torque} = \text{force} \times \text{distance} \doteq \underline{\underline{FL}}$

$$\doteq (MLT^{-2})(L) \doteq \underline{\underline{ML^2T^{-2}}}$$

(e) $\text{work} = \text{force} \times \text{distance} \doteq \underline{\underline{FL}}$

$$\doteq (MLT^{-2})(L) \doteq \underline{\underline{ML^2T^{-2}}}$$

1.7

1.7 If u is a velocity, x a length, and t a time, what are the dimensions (in the MLT system) of **(a)** $\partial u/\partial t$, **(b)** $\partial^2 u/\partial x \partial t$, and **(c)** $\int (\partial u/\partial t)\, dx$?

(a) $\frac{\partial u}{\partial t} \doteq \frac{LT^{-1}}{T} \doteq \underline{\underline{LT^{-2}}}$

(b) $\frac{\partial^2 u}{\partial x \partial t} \doteq \frac{LT^{-1}}{(L)(T)} \doteq \underline{\underline{T^{-2}}}$

(c) $\int \frac{\partial u}{\partial t}\, dx \doteq \frac{(LT^{-1})}{T}(L) \doteq \underline{\underline{L^2T^{-2}}}$

1.8

1.8 Verify the dimensions, in both the *FLT* system and the *MLT* system, of the following quantities which appear in Table 1.1: **(a)** acceleration, **(b)** stress, **(c)** moment of a force, **(d)** volume, and **(e)** work.

(a) $\text{acceleration} = \dfrac{\text{velocity}}{\text{time}} \doteq \dfrac{L}{T^2} \doteq \underline{\underline{LT^{-2}}}$

(b) $\text{stress} = \dfrac{\text{force}}{\text{area}} \doteq \dfrac{F}{L^2} \doteq \underline{\underline{FL^{-2}}}$

Since $F \doteq MLT^{-2}$,

$\text{stress} \doteq \dfrac{MLT^{-2}}{L^2} = \underline{\underline{ML^{-1}T^{-2}}}$

(c) $\text{moment of a force} = \text{force} \times \text{distance} \doteq \underline{\underline{FL}}$

$\doteq (MLT^{-2})L \doteq \underline{\underline{ML^2T^{-2}}}$

(d) $\text{volume} = (\text{length})^3 \doteq \underline{\underline{L^3}}$

(e) $\text{work} = \text{force} \times \text{distance} \doteq \underline{\underline{FL}}$

$\doteq (MLT^{-2})L \doteq \underline{\underline{ML^2T^{-2}}}$

1.9

1.9 If p is a pressure, V a velocity, and ρ a fluid density, what are the dimensions (in the MLT system) of (a) p/ρ, (b) $pV\rho$, and (c) $p/\rho V^2$?

(a) $$\frac{p}{\rho} \doteq \frac{ML^{-1}T^{-2}}{ML^{-3}} \doteq \underline{\underline{L^2T^{-2}}}$$

(b) $$pV\rho \doteq (ML^{-1}T^{-2})(LT^{-1})(ML^{-3}) \doteq \underline{\underline{M^2L^{-3}T^{-3}}}$$

(c) $$\frac{p}{\rho V^2} \doteq \frac{ML^{-1}T^{-2}}{(ML^{-3})(LT^{-1})^2} \doteq M^0L^0T^0 \ (\underline{\underline{\text{dimensionless}}})$$

1.10

1.10 If P is a force and x a length, what are the dimensions (in the FLT system) of **(a)** dP/dx, **(b)** d^3P/dx^3, and **(c)** $\int P\,dx$?

(a) $\dfrac{dP}{dx} \doteq \dfrac{F}{L} \doteq \underline{\underline{FL^{-2}}}$

(b) $\dfrac{d^3P}{dx^3} \doteq \dfrac{F}{L^3} \doteq \underline{\underline{FL^{-3}}}$

(c) $\int P\,dx \doteq \underline{\underline{FL}}$

1.11

1.11 If V is a velocity, ℓ a length, and ν a fluid property (the kinematic viscosity) having dimensions of L^2T^{-1}, which of the following combinations are dimensionless: (a) $V\ell\nu$, (b) $V\ell/\nu$, (c) $V^2\nu$, (d) $V/\ell\nu$?

(a) $V\ell\nu \doteq (LT^{-1})(L)(L^2T^{-1}) \doteq L^4T^{-2}$ (not dimensionless)

(b) $\frac{V\ell}{\nu} \doteq \frac{(LT^{-1})(L)}{(L^2T^{-1})} \doteq L^0T^0$ (dimensionless)

(c) $V^2\nu \doteq (LT^{-1})^2(L^2T^{-1}) \doteq L^4T^{-3}$ (not dimensionless)

(d) $\frac{V}{\ell\nu} \doteq \frac{(LT^{-1})}{(L)(L^2T^{-1})} \doteq L^{-2}$ (not dimensionless)

1.12

1.12 If V is a velocity, determine the dimensions of Z, α, and G, which appear in the dimensionally homogeneous equation

$$V = Z(\alpha - 1) + G$$

$$V = Z(\alpha - 1) + G$$

$$[LT^{-1}] \doteq [Z][\alpha - 1] + [G]$$

Since each term in the equation must have the same dimensions, it follows that

$$Z \doteq \underline{\underline{LT^{-1}}}$$

$$\alpha \doteq \underline{\underline{F^0L^0T^0}}$$ (dimensionless since combined with a number)

$$G \doteq \underline{\underline{LT^{-1}}}$$

1.13

1.13 The volume rate of flow, Q, through a pipe containing a slowly moving liquid is given by the equation

$$Q = \frac{\pi R^4 \Delta p}{8\mu \ell}$$

where R is the pipe radius, Δp the pressure drop along the pipe, μ a fluid property called viscosity $(FL^{-2}T)$, and ℓ the length of pipe. What are the dimensions of the constant $\pi/8$? Would you classify this equation as a general homogeneous equation? Explain.

$$[L^3 T^{-1}] \doteq \left[\frac{\pi}{8}\right] \frac{[L^4][FL^{-2}]}{[FL^{-2}T][L]}$$

$$[L^3 T^{-1}] \doteq \left[\frac{\pi}{8}\right] [L^3 T^{-1}]$$

The constant $\pi/8$ is dimensionless, and the equation is a general homogeneous equation that is valid in any consistent unit system. Yes.

1.14

1.14 According to information found in an old hydraulics book, the energy loss per unit weight of fluid flowing through a nozzle connected to a hose can be estimated by the formula

$$h = (0.04 \text{ to } 0.09)(D/d)^4 V^2/2g$$

where h is the energy loss per unit weight, D the hose diameter, d the nozzle tip diameter, V the fluid velocity in the hose, and g the acceleration of gravity. Do you think this equation is valid in any system of units? Explain.

$$h = (0.04 \text{ to } 0.09)\left(\frac{D}{d}\right)^4 \frac{V^2}{2g}$$

$$\left[\frac{FL}{F}\right] \doteq \left[0.04 \text{ to } 0.09\right]\left[\frac{L^4}{L^4}\right]\left[\frac{1}{2}\right]\left[\frac{L^2}{T^2}\right]\left[\frac{T^2}{L}\right]$$

$$[L] \doteq [0.04 \text{ to } 0.09][L]$$

Since each term in the equation must have the same dimensions, the constant term (0.04 to 0.09) must be dimensionless. Thus, the equation is a general homogeneous equation that is valid in any system of units. Yes.

1.15

1.15 The pressure difference, Δp, across a partial blockage in an artery (called a *stenosis*) is approximated by the equation

$$\Delta p = K_v \frac{\mu V}{D} + K_u \left(\frac{A_0}{A_1} - 1\right)^2 \rho V^2$$

where V is the blood velocity, μ the blood viscosity ($FL^{-2}T$), ρ the blood density (ML^{-3}), D the artery diameter, A_0 the area of the unobstructed artery, and A_1 the area of the stenosis. Determine the dimensions of the constants K_v and K_u. Would this equation be valid in any system of units?

$$\Delta p = K_v \frac{\mu V}{D} + K_u\left[\frac{A_0}{A_1} - 1\right]^2 \rho V^2$$

$$\left[FL^{-2}\right] \doteq \left[K_v\right]\left[\left(\frac{FT}{L^2}\right)\left(\frac{L}{T}\right)\left(\frac{1}{L}\right)\right] + \left[K_u\right]\left[\frac{(L^2)}{(L^2)} - 1\right]^2\left[\frac{FT^2}{L^4}\right]\left[\frac{L}{T}\right]^2$$

$$\left[FL^{-2}\right] \doteq \left[K_v\right]\left[FL^{-2}\right] + \left[K_u\right]\left[FL^{-2}\right]$$

Since each term must have the same dimensions, K_v and K_u are dimensionless. Thus, the equation is a general homogeneous equation that would be valid in any consistent system of units. Yes.

1.16

1.16 Assume that the speed of sound, c, in a fluid depends on an elastic modulus, E_v, with dimensions FL^{-2}, and the fluid density, ρ, in the form $c = (E_v)^a(\rho)^b$. If this is to be a dimensionally homogeneous equation, what are the values for a and b? Is your result consistent with the standard formula for the speed of sound? (See Eq. 1.19.)

$$c = (E_v)^a (\rho)^b$$

Since $c \doteq LT^{-1}$ $\quad E_v \doteq FL^{-2}$ $\quad \rho = FL^{-4}T^2$

$$\left[\frac{L}{T}\right] \doteq \left[\frac{F^a}{L^{-2a}}\right]\left[\frac{F^b T^{2b}}{L^{-4b}}\right] \qquad (1)$$

For a dimensionally homogeneous equation each term in the equation must have the same dimensions. Thus, the right hand side of Eq. (1) must have the dimensions of LT^{-1}. Therefore,

$$a + b = 0 \quad \text{(to eliminate } F\text{)}$$
$$2b = -1 \quad \text{(to satisfy condition on } T\text{)}$$
$$2a + 4b = -1 \quad \text{(to satisfy condition on } L\text{)}$$

It follows that $a = \frac{1}{2}$ and $b = -\frac{1}{2}$

So that

$$c = \sqrt{\frac{E_v}{\rho}}$$

This result is consistent with the standard formula for the speed of sound. Yes.

1.17

1.17 A formula to estimate the volume rate of flow, Q, flowing over a dam of length, B, is given by the equation

$$Q = 3.09BH^{3/2}$$

where H is the depth of the water above the top of the dam (called the head). This formula gives Q in ft^3/s when B and H are in feet. Is the constant, 3.09, dimensionless? Would this equation be valid if units other than feet and seconds were used?

$$Q = 3.09\, B\, H^{3/2}$$

$$[L^3T^{-1}] \doteq [3.09][L][L]^{3/2}$$

$$[L^3T^{-1}] \doteq [3.09][L]^{5/2}$$

Since each term in the equation must have the same dimensions the constant 3.09 must have dimensions of $L^{1/2}T^{-1}$ and is therefore not dimensionless. No.

Since the constant has dimensions its value will change with a change in units. No.

1.18

1.18 The force, P, that is exerted on a spherical particle moving slowly through a liquid is given by the equation

$$P = 3\pi\mu DV$$

where μ is a fluid property (viscosity) having dimensions of $FL^{-2}T$, D is the particle diameter, and V is the particle velocity. What are the dimensions of the constant, 3π? Would you classify this equation as a general homogeneous equation?

$$P = 3\pi\mu D V$$

$$[F] \doteq [3\pi][FL^{-2}T][L][LT^{-1}]$$

$$[F] \doteq [3\pi][F]$$

$\therefore$ 3π is dimensionless, and the equation is a general homogeneous equation. Yes.

1.20

1.20 Make use of Table 1.3 to express the following quantities in SI units: **(a)** 10.2 in./min, **(b)** 4.81 slugs, **(c)** 3.02 lb, **(d)** 73.1 ft/s², **(e)** 0.0234 lb·s/ft².

(a) $$10.2\ \frac{in.}{min} = \left(10.2\ \frac{in.}{min}\right)\left(2.540\times10^{-2}\ \frac{m}{in.}\right)\left(\frac{1\ min}{60\ s}\right)$$

$$= 4.32\times10^{-3}\ \frac{m}{s} = \underline{\underline{4.32\ \frac{mm}{s}}}$$

(b) $$4.81\ slugs = (4.81\ slugs)\left(1.459\times10\ \frac{kg}{slug}\right) = \underline{\underline{70.2\ kg}}$$

(c) $$3.02\ lb = (3.02\ lb)\left(4.448\ \frac{N}{lb}\right) = \underline{\underline{13.4\ N}}$$

(d) $$73.1\ \frac{ft}{s^2} = \left(73.1\ \frac{ft}{s^2}\right)\left(3.048\times10^{-1}\ \frac{\frac{m}{s^2}}{\frac{ft}{s^2}}\right) = \underline{\underline{22.3\ \frac{m}{s^2}}}$$

(e) $$0.0234\ \frac{lb\cdot s}{ft^2} = \left(0.0234\ \frac{lb\cdot s}{ft^2}\right)\left(4.788\times10\ \frac{\frac{N\cdot s}{m^2}}{\frac{lb\cdot s}{ft^2}}\right)$$

$$= \underline{\underline{1.12\ \frac{N\cdot s}{m^2}}}$$

1.15.

1.21

1.21 Make use of Table 1.4 to express the following quantities in BG units: **(a)** 14.2 km, **(b)** 8.14 N/m³, **(c)** 1.61 kg/m³, **(d)** 0.0320 N·m/s, **(e)** 5.67 mm/hr.

(a) $14.2\ km = (14.2\times10^{3}\ m)\left(3.281\ \frac{ft}{m}\right) = \underline{\underline{4.66\times10^{4}\ ft}}$

(b) $8.14\ \frac{N}{m^3} = \left(8.14\ \frac{N}{m^3}\right)\left(6.366\times10^{-3}\ \frac{\frac{lb}{ft^3}}{\frac{N}{m^3}}\right) = \underline{\underline{5.18\times10^{-2}\ \frac{lb}{ft^3}}}$

(c) $1.61\ \frac{kg}{m^3} = \left(1.61\ \frac{kg}{m^3}\right)\left(1.940\times10^{-3}\ \frac{\frac{slugs}{ft^3}}{\frac{kg}{m^3}}\right) = \underline{\underline{3.12\times10^{-3}\ \frac{slugs}{ft^3}}}$

(d) $0.0320\ \frac{N\cdot m}{s} = \left(0.0320\ \frac{N\cdot m}{s}\right)\left(7.376\times10^{-1}\ \frac{\frac{ft\cdot lb}{s}}{\frac{N\cdot m}{s}}\right)$

$= \underline{\underline{2.36\times10^{-2}\ \frac{ft\cdot lb}{s}}}$

(e) $5.67\ \frac{mm}{hr} = \left(5.67\times10^{-3}\ \frac{m}{hr}\right)\left(3.281\ \frac{ft}{m}\right)\left(\frac{1\ hr}{3600\ s}\right)$

$= \underline{\underline{5.17\times10^{-6}\ \frac{ft}{s}}}$

1.22

1.22 Express the following quantities in SI units: **(a)** 160 acre, **(b)** 15 gallons (U.S.), **(c)** 240 miles, **(d)** 79.1 hp, **(e)** 60.3 °F.

(a) $160 \text{ acre} = (160 \text{ acre})\left(4.356 \times 10^4 \frac{ft^2}{acre}\right)\left(9.290 \times 10^{-2} \frac{m^2}{ft^2}\right)$

$= \underline{\underline{6.47 \times 10^5 \, m^2}}$

(b) $15 \text{ gallons} = (15 \text{ gallons})\left(3.785 \frac{liters}{gallon}\right)\left(10^{-3} \frac{m^3}{liter}\right) = \underline{\underline{56.8 \times 10^{-2} \, m^3}}$

(c) $240 \text{ mi} = (240 \text{ mi})\left(5280 \frac{ft}{mi}\right)\left(3.048 \times 10^{-1} \frac{m}{ft}\right) = \underline{\underline{3.86 \times 10^5 \, m}}$

(d) $79.1 \text{ hp} = (79.1 \text{ hp})\left(550 \frac{ft \cdot lb / s}{hp}\right)\left(1.356 \frac{J}{ft \cdot lb}\right) = 5.90 \times 10^4 \, \frac{J}{s}$

and $1 \, \frac{J}{s} = 1 \, W$ so that

$79.1 \text{ hp} = \underline{\underline{5.90 \times 10^4 \, W}}$

(e) $T_C = \frac{5}{9}(60.3°F - 32) = 15.7°C$

$= 15.7°C + 273 = \underline{\underline{289 \, K}}$

1.18

1.23

1.23 For Table 1.3 verify the conversion relationships for: **(a)** area, **(b)** density, **(c)** velocity, and **(d)** specific weight. Use the basic conversion relationships: 1 ft = 0.3048 m; 1 lb = 4.4482 N; and 1 slug = 14.594 kg.

(a) $$1\ ft^2 = (1\ ft^2)\left[(0.3048)^2 \frac{m^2}{ft^2}\right] = 0.09290\ m^2$$

Thus, multiply ft^2 by $\underline{\underline{9.290\ E-2}}$ to convert to m^2.

(b) $$1\ \frac{slug}{ft^3} = \left(1\ \frac{slug}{ft^3}\right)\left(14.594\ \frac{kg}{slug}\right)\left[\frac{1\ ft^3}{(0.3048)^3 m^3}\right]$$

$$= 515.4\ \frac{kg}{m^3}$$

Thus, multiply $slugs/ft^3$ by $\underline{\underline{5.154\ E+2}}$ to convert to kg/m^3.

(c) $$1\ \frac{ft}{s} = \left(1\ \frac{ft}{s}\right)\left(0.3048\ \frac{m}{ft}\right) = 0.3048\ \frac{m}{s}$$

Thus, multiply ft/s by $\underline{\underline{3.048\ E-1}}$ to convert to m/s.

(d) $$1\ \frac{lb}{ft^3} = \left(1\ \frac{lb}{ft^3}\right)\left(4.4482\ \frac{N}{lb}\right)\left[\frac{1\ ft^3}{(0.3048)^3 m^3}\right]$$

$$= 157.1\ \frac{N}{m^3}$$

Thus, multiply lb/ft^3 by $\underline{\underline{1.571\ E+2}}$ to convert to N/m^3.

1.24

1.24 For Table 1.4 verify the conversion relationships for: **(a)** acceleration, **(b)** density, **(c)** pressure, and **(d)** volume flowrate. Use the basic conversion relationships: 1 m = 3.2808 ft; 1 N = 0.22481 lb; and 1 kg = 0.068521 slug.

(a) $$1\ \frac{m}{s^2} = \left(1\ \frac{m}{s^2}\right)\left(3.2808\ \frac{ft}{m}\right) = 3.281\ \frac{ft}{s^2}$$

Thus, multiply m/s^2 by 3.281 to convert to ft/s^2.

(b) $$1\ \frac{kg}{m^3} = \left(1\ \frac{kg}{m^3}\right)\left(0.068521\ \frac{slugs}{kg}\right)\left[\frac{1\ m^3}{(3.2808)^3\ ft^3}\right]$$

$$= 1.940 \times 10^{-3}\ \frac{slugs}{ft^3}$$

Thus, multiply kg/m^3 by 1.940 E−3 to convert to $slugs/ft^3$.

(c) $$1\ \frac{N}{m^2} = \left(1\ \frac{N}{m^2}\right)\left(0.22481\ \frac{lb}{N}\right)\left[\frac{1\ m^2}{(3.2808)^2\ ft^2}\right]$$

$$= 2.089 \times 10^{-2}\ \frac{lb}{ft^2}$$

Thus, multiply N/m^2 by 2.089 E−2 to convert to lb/ft^2.

(d) $$1\ \frac{m^3}{s} = \left(1\ \frac{m^3}{s}\right)\left[(3.2808)^3\ \frac{ft^3}{m^3}\right] = 35.31\ \frac{ft^3}{s}$$

Thus, multiply m^3/s by 3.531 E+1 to convert to ft^3/s.

1.25

1.25 Water flows from a large drainage pipe at a rate of 1200 gal/min. What is this volume rate of flow in (a) m^3/s, (b) liters/min, and (c) ft^3/s?

(a)

$$\text{flowrate} = \left(1200\ \frac{gal}{min}\right)\left(6.309 \times 10^{-5}\ \frac{\frac{m^3}{s}}{\frac{gal}{min}}\right)$$

$$= \underline{\underline{7.57 \times 10^{-2}\ \frac{m^3}{s}}}$$

(b) Since 1 liter $= 10^{-3}\ m^3$,

$$\text{flowrate} = \left(7.57 \times 10^{-2}\ \frac{m^3}{s}\right)\left(\frac{10^3\ liters}{m^3}\right)\left(\frac{60\,s}{min}\right)$$

$$= \underline{\underline{4540\ \frac{liters}{min}}}$$

(c)

$$\text{flowrate} = \left(7.57 \times 10^{-2}\ \frac{m^3}{s}\right)\left(3.531 \times 10\ \frac{\frac{ft^3}{s}}{\frac{m^3}{s}}\right)$$

$$= \underline{\underline{2.67\ \frac{ft^3}{s}}}$$

1.26

1.26 Dimensionless combinations of quantities (commonly called dimensionless parameters) play an important role in fluid mechanics. Make up five possible dimensionless parameters by using combinations of some of the quantities listed in Table 1.1.

Some possible examples:

$$\frac{\text{acceleration} \times \text{time}}{\text{velocity}} \doteq \frac{(LT^{-2})(T)}{(LT^{-1})} \doteq L^0T^0$$

$$\text{frequency} \times \text{time} \doteq (T^{-1})(T) \doteq T^0$$

$$\frac{(\text{velocity})^2}{\text{length} \times \text{acceleration}} \doteq \frac{(LT^{-1})^2}{(L)(LT^{-2})} \doteq L^0T^0$$

$$\frac{\text{force} \times \text{time}}{\text{momentum}} \doteq \frac{(F)(T)}{(MLT^{-1})} \doteq \frac{(F)(T)}{(FT^2L^{-1})(LT^{-1})} \doteq F^0L^0T^0$$

$$\frac{\text{density} \times \text{velocity} \times \text{length}}{\text{dynamic viscosity}} \doteq \frac{(ML^{-3})(LT^{-1})(L)}{ML^{-1}T^{-1}} \doteq M^0L^0T^0$$

1,23

1.27

1.27 An important dimensionless parameter in certain types of fluid flow problems is the *Froude number* defined as $V/\sqrt{g\ell}$, where V is a velocity, g the acceleration of gravity, and ℓ a length. Determine the value of the Froude number for $V = 10$ ft/s, $g = 32.2$ ft/s², and $\ell = 2$ ft. Recalculate the Froude number using SI units for V, g, and ℓ. Explain the significance of the results of these calculations.

In BG units,

$$\frac{V}{\sqrt{g\ell}} = \frac{10\ \frac{ft}{s}}{\sqrt{\left(32.2\ \frac{ft}{s^2}\right)(2\ ft)}} = \underline{\underline{1.25}}$$

In SI units:

$$V = \left(10\ \frac{ft}{s}\right)\left(0.3048\ \frac{m}{ft}\right) = 3.05\ \frac{m}{s}$$

$$g = 9.81\ \frac{m}{s^2}$$

$$\ell = (2\ ft)\left(0.3048\ \frac{m}{ft}\right) = 0.610\ m$$

Thus,

$$\frac{V}{\sqrt{g\ell}} = \frac{3.05\ \frac{m}{s}}{\sqrt{\left(9.81\ \frac{m}{s^2}\right)(0.610\ m)}} = \underline{\underline{1.25}}$$

The value of a dimensionless parameter is independent of the unit system.

1.29

1.29 A tank contains 500 kg of a liquid whose specific gravity is 2. Determine the volume of the liquid in the tank.

$$m = \rho \mathcal{V} = SG\, \rho_{H_2O} \mathcal{V}$$

Thus,

$$\mathcal{V} = m/(SG\, \rho_{H_2O}) = 500\,kg/((2)(999\,\frac{kg}{m^3}))$$

$$= \underline{\underline{0.250\,m^3}}$$

1.30

1.30 Clouds can weigh thousands of pounds due to their liquid water content. Often this content is measured in grams per cubic meter (g/m^3). Assume that a cumulus cloud occupies a volume of one cubic kilometer, and its liquid water content is 0.2 g/m^3. (a) What is the volume of this cloud in cubic miles? (b) How much does the water in the cloud weigh in pounds?

(a) $\mathcal{V}olume = 1\,(km)^3 = 10^9\,m^3$

Since $1\,m = 3.281\,ft$

$$\mathcal{V}olume = \frac{(10^9\,m^3)(3.281\,\frac{ft}{m})^3}{(5.280\times10^3\,\frac{ft}{mi})^3}$$

$$= \underline{\underline{0.240\,mi^3}}$$

(b) $\mathcal{W} = \gamma \times \mathcal{V}olume$

$$\gamma = \rho g = \left(0.2\,\frac{g}{m^3}\right)\left(10^{-3}\,\frac{kg}{g}\right)\left(9.81\,\frac{m}{s^2}\right) = 1.962\times10^{-3}\,\frac{N}{m^3}$$

$$\mathcal{W} = \left(1.962\times10^{-3}\,\frac{N}{m^3}\right)\left(10^9\,m^3\right) = 1.962\times10^6\,N$$

$$= \left(1.962\times10^6\,N\right)\left(2.248\times10^{-1}\,\frac{lb}{N}\right) = \underline{\underline{4.41\times10^5\,lb}}$$

1.21

1.31

1.31 A tank of oil has a mass of 25 slugs. **(a)** Determine its weight in pounds and in newtons at the earth's surface. **(b)** What would be its mass (in slugs) and its weight (in pounds) if located on the moon's surface where the gravitational attraction is approximately one-sixth that at the earth's surface?

(a) $$\text{weight} = \text{mass} \times g$$

$$= (25 \text{ slugs})\left(32.2 \frac{ft}{s^2}\right) = \underline{\underline{805 \text{ lb}}}$$

$$= (25 \text{ slugs})\left(14.59 \frac{kg}{slug}\right)\left(9.81 \frac{m}{s^2}\right) = \underline{\underline{3580 \text{ N}}}$$

(b) $$\text{mass} = \underline{\underline{25 \text{ slugs}}}$$ (mass does not depend on gravitational attraction)

$$\text{weight} = (25 \text{ slugs})\left(\frac{32.2 \frac{ft}{s^2}}{6}\right) = \underline{\underline{134 \text{ lb}}}$$

1.22

1.32

1.32 A certain object weighs 300 N at the earth's surface. Determine the mass of the object (in kilograms) and its weight (in newtons) when located on a planet with an acceleration of gravity equal to 4.0 ft/s^2.

$$\text{mass} = \frac{\text{weight}}{g}$$

$$= \frac{300 \text{ N}}{9.81 \frac{m}{s^2}} = \underline{\underline{30.6 \text{ kg}}}$$

For $g = 4.0 \text{ ft/s}^2$,

$$\text{weight} = (30.6 \text{ kg})\left(4.0 \frac{ft}{s^2}\right)\left(0.3048 \frac{m}{ft}\right)$$

$$= \underline{\underline{37.3 \text{ N}}}$$

1.33

1.33 The density of a certain type of jet fuel is 775 kg/m³. Determine its specific gravity and specific weight.

$$SG = \frac{\rho}{\rho_{H_2O} @ 4°C} = \frac{775 \frac{kg}{m^3}}{1000 \frac{kg}{m^3}} = \underline{\underline{0.775}}$$

$$\gamma = \rho g = \left(775 \frac{kg}{m^3}\right)\left(9.81 \frac{m}{s^2}\right) = \underline{\underline{7.60 \frac{kN}{m^3}}}$$

1.34

1.34 A *hydrometer* is used to measure the specific gravity of liquids. (See **Video V2.8.**) For a certain liquid a hydrometer reading indicates a specific gravity of 1.15. What is the liquid's density and specific weight? Express your answer in SI units.

$$SG = \frac{\rho}{\rho_{H_2O\,@4^\circ C}}$$

$$1.15 = \frac{\rho}{1000\ \frac{kg}{m^3}}$$

$$\rho = (1.15)\left(1000\ \frac{kg}{m^3}\right) = \underline{\underline{1150\ \frac{kg}{m^3}}}$$

$$\gamma = \rho g = \left(1150\ \frac{kg}{m^3}\right)\left(9.81\ \frac{m}{s^2}\right) = \underline{\underline{11.3\ \frac{kN}{m^3}}}$$

1.35

1.35 The specific weight of a certain liquid is 85.3 lb/ft³. Determine its density and specific gravity.

$$\rho = \frac{\gamma}{g} = \frac{85.3\ \frac{lb}{ft^3}}{32.2\ \frac{ft}{s^2}} = \underline{\underline{2.65\ \frac{slugs}{ft^3}}}$$

$$SG = \frac{\rho}{\rho_{H_2O}\ @\ 4^\circ C} = \frac{2.65\ \frac{slugs}{ft^3}}{1.94\ \frac{slugs}{ft^3}} = \underline{\underline{1.37}}$$

1.26

1.36

1.36 An open, rigid-walled, cylindrical tank contains 4 ft^3 of water at 40 °F. Over a 24-hour period of time the water temperature varies from 40 °F to 90 °F. Make use of the data in Appendix B to determine how much the volume of water will change. For a tank diameter of 2 ft, would the corresponding change in water depth be very noticeable? Explain.

mass of water $= \forall \times \rho$

where $\forall$ is the volume and ρ the density. Since the mass must remain constant as the temperature changes

$$\forall_{40°} \times \rho_{40°} = \forall_{90°} \times \rho_{90°} \qquad (1)$$

From Table B.1 $\rho_{H_2O\,@\,40°F} = 1.940 \frac{slugs}{ft^3}$

$\rho_{H_2O\,@\,90°F} = 1.931 \frac{slugs}{ft^3}$

Therefore, from Eq. (1)

$$\forall_{90°} = \frac{(4\,ft^3)(1.940\,\frac{slugs}{ft^3})}{1.931\,\frac{slugs}{ft^3}} = 4.0186\,ft^3$$

Thus, the increase in volume is

$$4.0186 - 4.000 = \underline{\underline{0.0186\,ft^3}}$$

The change in water depth, $\Delta \ell$, is equal to

$$\Delta \ell = \frac{\Delta \forall}{area} = \frac{0.0186\,ft^3}{\frac{\pi}{4}(2ft)^2} = 5.92 \times 10^{-3}\,ft = 0.0710\,in.$$

This small change in depth would not be very noticeable. $\underline{\underline{No}}$.

Note: A slightly different value for $\Delta \ell$ will be obtained if specific weight of water is used rather than density. This is due to the fact that there is some uncertainty in the fourth significant figure of these two values, and the solution is sensitive to this uncertainty.

1.38

1.38 A mountain climber's oxygen tank contains 1 lb of oxygen when he begins his trip at sea level where the acceleration of gravity is 32.174 ft/s^2. What is the weight of the oxygen in the tank when he reaches to top of Mt. Everest where the acceleration of gravity is 32.082 ft/s^2? Assume that no oxygen has been removed from the tank; it will be used on the descent portion of the climb.

$W = mg$

Let $(\ )_{sl}$ denote sea level and $(\ )_{MtE}$ denote the top of Mt. Everest

Thus,

$W_{sl} = 1\,lb = m_{sl}\, g_{sl}$ and

$W_{MtE} = m_{MtE}\, g_{MtE}$

However $m_{sl} = m_{MtE}$ so that since $m = \frac{W}{g}$,

$$m_{sl} = \frac{W_{sl}}{g_{sl}} = m_{MtE} = \frac{W_{MtE}}{g_{MtE}}$$

or

$$W_{MtE} = W_{sl}\frac{g_{MtE}}{g_{sl}} = 1\,lb\,\frac{32.082\ ft/s^2}{32.174\ ft/s^2} = \underline{\underline{0.9971\ lb}}$$

27 bi

1.29

1.39

1.39 The information on a can of pop indicates that the can contains 355 mL. The mass of a full can of pop is 0.369 kg while an empty can weighs 0.153 N. Determine the specific weight, density, and specific gravity of the pop and compare your results with the corresponding values for water at 20 °C. Express your results in SI units.

$$\gamma = \frac{\text{weight of fluid}}{\text{volume of fluid}} \qquad (1)$$

total weight = mass × g = $(0.369\ kg)(9.81\ \frac{m}{s^2}) = 3.62\ N$

weight of can = $0.153\ N$

Volume of fluid = $(355 \times 10^{-3}\ L)(10^{-3}\ \frac{m^3}{L}) = 355 \times 10^{-6}\ m^3$

Thus, from Eq. (1)

$$\gamma = \frac{3.62\ N - 0.153\ N}{355 \times 10^{-6}\ m^3} = \underline{\underline{9770\ \frac{N}{m^3}}}$$

$$\rho = \frac{\gamma}{g} = \frac{9770\ \frac{N}{m^3}}{9.81\ \frac{m}{s^2}} = 996\ \frac{N \cdot s^2}{m^4} = \underline{\underline{996\ \frac{kg}{m^3}}}$$

$$SG = \frac{\rho}{\rho_{H_2O@4°C}} = \frac{996\ \frac{kg}{m^3}}{1000\ \frac{kg}{m^3}} = \underline{\underline{0.996}}$$

For water at 20°C (see Table B.2 in Appendix B)

$$\gamma_{H_2O} = 9789\ \frac{N}{m^3}\ ;\ \rho_{H_2O} = 998.2\ \frac{kg}{m^3}\ ;\ SG = 0.9982$$

A comparison of these values for water with those for the pop shows that the specific weight, density, and specific gravity of the pop are all slightly lower than the corresponding values for water.

22bi

*1.40

*1.40 The variation in the density of water, ρ, with temperature, T, in the range 20 °C ≤ T ≤ 50 °C, is given in the following table.

Density (kg/m³)	998.2	997.1	995.7	994.1	992.2	990.2	988.1
Temperature (°C)	20	25	30	35	40	45	50

Use these data to determine an empirical equation of the form $\rho = c_1 + c_2T + c_3T^2$ which can be used to predict the density over the range indicated. Compare the predicted values with the data given. What is the density of water at 42.1 °C?

Fit the data to a second order polynomial using a standard curve-fitting program such as found in EXCEL. Thus,

$$\rho = 1001 - 0.0533T - 0.0041T^2 \qquad (1)$$

As shown in the table below, ρ (predicted) from Eq. (1) is in good agreement with ρ (given).

T, °C	ρ, kg/m^3	ρ, Predicted
20	998.2	998.3
25	997.1	997.1
30	995.7	995.7
35	994.1	994.1
40	992.2	992.3
45	990.2	990.3
50	988.1	988.1

At $T = 42.1$ °C

$$\rho = 1001 - 0.0533(42.1\,°C) - 0.0041(42.1\,°C)^2 = \underline{991.5\ \frac{kg}{m^3}}$$

236i

1.41

1.41 If 1 cup of cream having a density of 1005 kg/m³ is turned into 3 cups of whipped cream, determine the specific gravity and specific weight of the whipped cream.

Mass of cream, $m = \left(1005 \frac{kg}{m^3}\right) \times \left(\forall_{cup}\right)$

where $\forall$ ~ volume.

Since $m_{cream} = m_{\substack{whipped \\ cream}}$

$$\rho_{\substack{whipped \\ cream}} = \frac{m_{\substack{whipped \\ cream}}}{\forall_{3\ cups}} = \frac{\left(1005 \frac{kg}{m^3}\right)\forall_{cup}}{\forall_{3\ cups}}$$

$$= \frac{1005 \frac{kg}{m^3}}{3} = 335 \frac{kg}{m^3}$$

$$SG = \frac{\rho_{\substack{whipped \\ cream}}}{\rho_{H_2O\ @\ 4°C}} = \frac{335 \frac{kg}{m^3}}{1000 \frac{kg}{m^3}} = \underline{\underline{0.335}}$$

$$\gamma_{\substack{whipped \\ cream}} = \rho_{\substack{whipped \\ cream}} \times g = \left(335 \frac{kg}{m^3}\right)\left(9.81 \frac{m}{s^2}\right)$$

$$= \underline{\underline{3290 \frac{N}{m^3}}}$$

2865

1.42

1.42 A liquid when poured into a graduated cylinder is found to weigh 8 N when occupying a volume of 500 ml (milliliters). Determine its specific weight, density, and specific gravity.

$$\gamma = \frac{\text{weight}}{\text{volume}} = \frac{8\,N}{(0.500\,\ell)\left(10^{-3}\,\frac{m^3}{\ell}\right)} = \underline{\underline{16.0\,\frac{kN}{m^3}}}$$

$$\rho = \frac{\gamma}{g} = \frac{16 \times 10^3\,\frac{N}{m^3}}{9.81\,\frac{m}{s^2}} = \underline{\underline{1.63 \times 10^3\,\frac{kg}{m^3}}}$$

$$SG = \frac{\rho}{\rho_{H_2O}\,@\,4°C} = \frac{1.63 \times 10^3\,\frac{kg}{m^3}}{10^3\,\frac{kg}{m^3}} = \underline{\underline{1.63}}$$

1.44

1.44 Determine the mass of air in a 2 m^3 tank if the air is at room temperature, 20 °C, and the absolute pressure within the tank is 200 kPa (abs).

$m = \rho \mathcal{V}$ where $\mathcal{V} = 2\,m^3$ and

$\rho = p/RT$ with $T = 20°C = (20+273)\,K = 293\,K$
and $p = 200\,kPa = 200 \times 10^3 \frac{N}{m^2}$

Thus,

$$\rho = \left(200 \times 10^3 \frac{N}{m^2}\right) \Big/ \left[\left(2.869 \times 10^2 \frac{N \cdot m}{kg \cdot K}\right)(293\,K)\right]$$

$$= 2.38 \frac{kg}{m^3}$$

Hence,

$$m = \rho \mathcal{V} = 2.38 \frac{kg}{m^3}(2\,m^3) = \underline{\underline{4.76\,kg}}$$

3 | 6i

1.45

1.45 Nitrogen is compressed to a density of 4 kg/m³ under an absolute pressure of 400 kPa. Determine the temperature in degrees Celsius.

$$T = \frac{p}{\rho R} = \frac{400 \times 10^{3} \frac{N}{m^2}}{\left(4 \frac{kg}{m^3}\right)\left(296.8 \frac{J}{kg \cdot K}\right)} = 337\ K$$

$$T_c = T_K - 273 = 337\,K - 273 = \underline{\underline{64\ °C}}$$

1.46

1.46 The temperature and pressure at the surface of Mars during a Martian spring day were determined to be −50 °C and 900 Pa, respectively. **(a)** Determine the density of the Martian atmosphere for these conditions if the gas constant for the Martian atmosphere is assumed to be equivalent to that of carbon dioxide. **(b)** Compare the answer from part (a) with the density of the earth's atmosphere during a spring day when the temperature is 18 °C and the pressure 101.6 kPa (abs).

$$(a)\quad \rho_{Mars} = \frac{p}{RT} = \frac{900 \frac{N}{m^2}}{\left(188.9 \frac{J}{kg \cdot K}\right)\left[(-50°C + 273)K\right]} = \underline{\underline{0.0214 \frac{kg}{m^3}}}$$

$$(b)\quad \rho_{earth} = \frac{p}{RT} = \frac{101.6 \times 10^{3} \frac{N}{m^2}}{\left(286.9 \frac{J}{kg \cdot K}\right)\left[(18°C + 273)K\right]} = 1.22 \frac{kg}{m^3}$$

Thus,

$$\frac{\rho_{Mars}}{\rho_{earth}} = \frac{0.0214 \frac{kg}{m^3}}{1.22 \frac{kg}{m^3}} = 0.0175 = \underline{\underline{1.75\%}}$$

1.47

1.47 A closed tank having a volume of 2 ft³ is filled with 0.30 lb of a gas. A pressure gage attached to the tank reads 12 psi when the gas temperature is 80 °F. There is some question as to whether the gas in the tank is oxygen or helium. Which do you think it is? Explain how you arrived at your answer.

Density of gas in tank $\rho = \frac{\text{weight}}{g \times \text{volume}} = \frac{0.30\ lb}{\left(32.2\ \frac{ft}{s^2}\right)(2\ ft^3)}$

$= 4.66 \times 10^{-3}\ \frac{slugs}{ft^3}$

Since $\rho = \frac{p}{RT}$ with $p = (12 + 14.7)\ psia$

(atmospheric pressure assumed to be $\approx 14.7\ psia$)

and with $T = (80°F + 460)\ °R$ it follows that

$$\rho = \frac{\left(26.7\ \frac{lb}{in.^2}\right)\left(144\ \frac{in.^2}{ft^2}\right)}{R\ (540°R)} = \frac{7.12}{R}\ \frac{slugs}{ft^3} \qquad (1)$$

From Table 1.7 $R = 1.554 \times 10^3$ for oxygen

and $R = 1.242 \times 10^4\ \frac{ft \cdot lb}{slug \cdot °R}$ for helium.

Thus, from Eq. (1) if the gas is oxygen

$$\rho = \frac{7.12}{1.554 \times 10^3}\ \frac{slugs}{ft^3} = 4.58 \times 10^{-3}\ \frac{slugs}{ft^3}$$

and for helium

$$\rho = \frac{7.12}{1.242 \times 10^4} = 5.73 \times 10^{-4}\ \frac{slugs}{ft^3}$$

A comparison of these values with the actual density of the gas in the tank indicates that the gas must be <u>oxygen</u>.

1.48

1.48 A tire having a volume of 3 ft³ contains air at a gage pressure of 26 psi and a temperature of 70 °F. Determine the density of the air and the weight of the air contained in the tire.

$$\rho = \frac{p}{RT} = \frac{\left(26\,\frac{lb}{in.^2} + 14.7\,\frac{lb}{in.^2}\right)\left(144\,\frac{in.^2}{ft^2}\right)}{\left(1716\,\frac{ft\cdot lb}{slug\cdot{}^\circ R}\right)\left[(70^\circ F + 460)\,^\circ R\right]} = \underline{\underline{6.44 \times 10^{-3}\,\frac{slugs}{ft^3}}}$$

$$\text{weight} = \rho g \times \text{volume} = \left(6.44 \times 10^{-3}\,\frac{slugs}{ft^3}\right)\left(32.2\,\frac{ft}{s^2}\right)\left(3\,ft^3\right)$$

$$= \underline{\underline{0.622\ lb}}$$

1.49

1.49 A compressed air tank contains 5 kg of air at a temperature of 80 °C. A gage on the tank reads 300 kPa. Determine the volume of the tank.

$$\text{volume} = \frac{\text{mass}}{\rho}$$

$$\rho = \frac{p}{RT} = \frac{(300 + 101) \times 10^3 \ \frac{N}{m^2}}{\left(286.9 \ \frac{J}{kg \cdot K}\right)\left[(80°C + 273)K\right]} = 3.96 \ \frac{kg}{m^3}$$

$$\text{volume} = \frac{5 \ kg}{3.96 \ \frac{kg}{m^3}} = \underline{\underline{1.26 \ m^3}}$$

1.50

1.50 A rigid tank contains air at a pressure of 90 psia and a temperature of 60 °F. By how much will the pressure increase as the temperature is increased to 110 °F?

$$p = \rho R T \qquad (\text{Eq. } 1.8)$$

For a rigid closed tank the air mass and volume are constant so $\rho =$ constant. Thus, from Eq. 1.8 (with R constant)

$$\frac{p_1}{T_1} = \frac{p_2}{T_2} \qquad (1)$$

where $p_1 = 90$ psia, $T_1 = 60°F + 460 = 520°R$, and $T_2 = 110°F + 460 = 570°R$. From Eq. (1)

$$p_2 = \frac{T_2}{T_1} p_1 = \left(\frac{570°R}{520°R}\right)(90 \text{ psia}) = \underline{\underline{98.7 \text{ psia}}}$$

1.51

1.51 The density of oxygen contained in a tank is 2.0 kg/m^3 when the temperature is 25 °C. Determine the gage pressure of the gas if the atmospheric pressure is 97 kPa.

$$p = \rho R T = \left(2.0\ \frac{kg}{m^3}\right)\left(259.8\ \frac{J}{kg \cdot K}\right)\left[(25°C + 273)K\right]$$

$$= 155\ kPa\ (abs)$$

$$p\ (gage) = p_{abs} - p_{atm} = 155\ kPa - 97\ kPa = \underline{\underline{58\ kPa}}$$

1.52

1.52 The helium-filled blimp shown in Fig. P1.52 is used at various athletic events. Determine the number of pounds of helium within it if its volume is 68,000 ft^3 and the temperature and pressure are 80 °F and 14.2 psia, respectively.

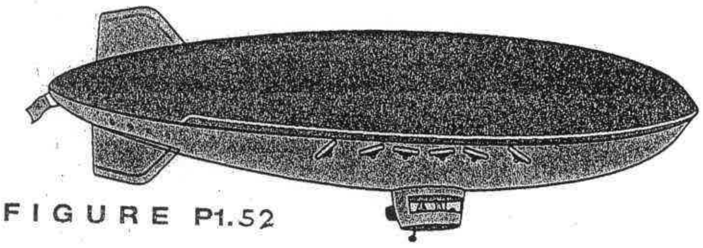


FIGURE P1.52

$\mathcal{W} = \gamma \mathcal{V}$ where $\mathcal{V} = 68{,}000\,ft^3$ and $\gamma = \rho g = (p/RT)g$

Thus,

$$\gamma = \left[14.2\,\frac{lb}{in.^2}\left(144\,\frac{in.^2}{ft^2}\right)\Big/\left(\left(1.242\times10^4\,\frac{ft\cdot lb}{slug\cdot {}^\circ R}\right)(80+460)^\circ R\right)\right](32.2\,\frac{ft}{s^2})$$

$$= 9.82\times10^{-3}\,\frac{slug}{ft^2\cdot s^2}\left(1\,lb/(slug\,ft/s^2)\right) = 9.82\times10^{-3}\,\frac{lb}{ft^3}$$

Hence,

$$\mathcal{W} = 9.82\times10^{-3}\,\frac{lb}{ft^3}\,(68{,}000\,ft^3) = \underline{\underline{668\,lb}}$$

34 bi

*1.53

*1.53 Develop a computer program for calculating the density of an ideal gas when the gas pressure in pascals (abs), the temperature in degrees Celsius, and the gas constant in J/kg · K are specified. Plot the density of helium as a function of temperature from 0 °C to 200 °C and pressures of 50, 100, 150, and 200 kPa (abs).

For an ideal gas

$$p = \rho R T$$

so that

$$\rho = \frac{p}{RT}$$

where p is absolute pressure, R the gas constant, and T is absolute temperature. Thus, if the temperature is in °C then

$$T = °C + 273.15$$

A spreadsheet (EXCEL) program for calculating ρ follows.

This program calculates the density of an ideal gas				
when the absolute pressure in Pascals, the temperature				
in degrees C, and the gas constant in J/kg·K are specified.				
To use, replace current values with desired values of				
temperature, pressure, and gas constant.				
A	B	C	D	
Pressure,	Temperature,	Gas constant,	Density,	
Pa	°C	J/kg·K	kg/m³	
1.01E+05	15	286.9	1.23	Row 10

Formula:
=A10/((B10+273.15)*C10)

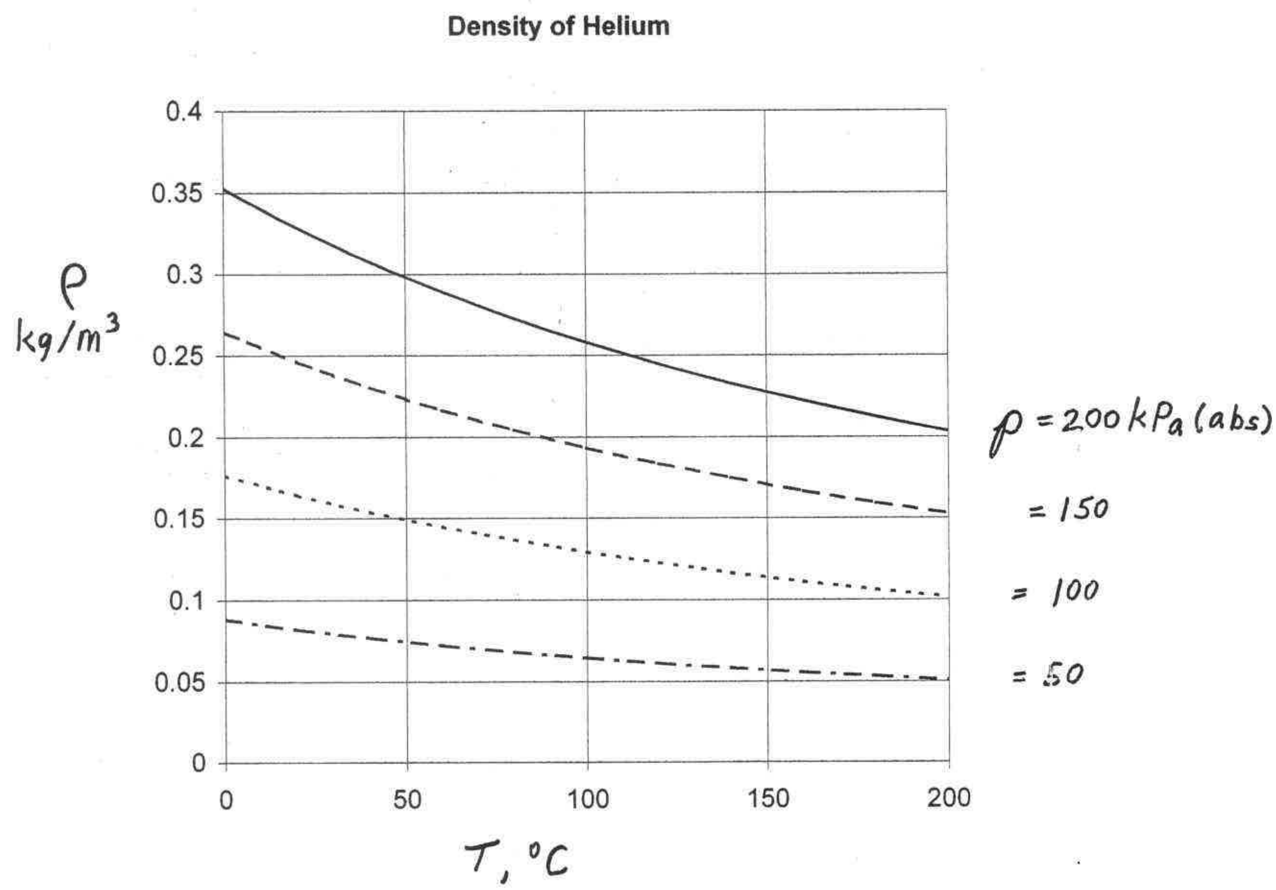
Example: Calculate ρ for $p = 200$ kPa, temperature = 20°C, and $R = 287$ J/kg·K.

A	B	C	D	
Pressure,	Temperature,	Gas constant,	Density,	
Pa	°C	J/kg·K	kg/m³	
2.00E+05	20	287	2.38	Row 10

(con't)

*1.53 (con't)

The density of helium is plotted in the graph below.



36 bi

1.55

1.55 For flowing water, what is the magnitude of the velocity gradient needed to produce a shear stress of 1.0 N/m^2?

$$\tau = \mu \frac{du}{dy} \quad \text{where } \mu = 1.12 \times 10^{-3} \frac{N \cdot s}{m^2} \text{ and } \tau = 1.0 \frac{N}{m^2}$$

Thus,

$$\frac{du}{dy} = \frac{\tau}{\mu} = \frac{1.0 \frac{N}{m^2}}{1.12 \times 10^{-3} \frac{N \cdot s}{m^2}} = \underline{\underline{893 \frac{1}{s}}}$$

1.56

1.56 Make use of the data in Appendix B to determine the dynamic viscosity of glycerin at 85 °F. Express your answer in both SI and BG units.

$$T_c = \frac{5}{9}(T_F - 32) = \frac{5}{9}(85°F - 32) = 29.4°C$$

From Fig. B.1 in Appendix B:

$$\mu \,(\text{glycerin at } 85°F\,(29.4°C)) \approx \underline{\underline{0.6 \frac{N \cdot s}{m^2}}} \quad (\text{SI units})$$

$$\mu \approx \left(0.6 \frac{N \cdot s}{m^2}\right)\left(2.089 \times 10^{-2} \frac{\frac{lb \cdot s}{ft^2}}{\frac{N \cdot s}{m^2}}\right) \approx \underline{\underline{1.3 \times 10^{-2} \frac{lb \cdot s}{ft^2}}} \quad (\text{BG units})$$

42 bi

1.57

1.57 Make use of the data in Appendix B to determine the dynamic viscosity of mercury at 75 °F. Express your answer in BG units.

$$T_C = \frac{5}{9}(T_F - 32) = \frac{5}{9}(75°F - 32) = 23.9°C$$

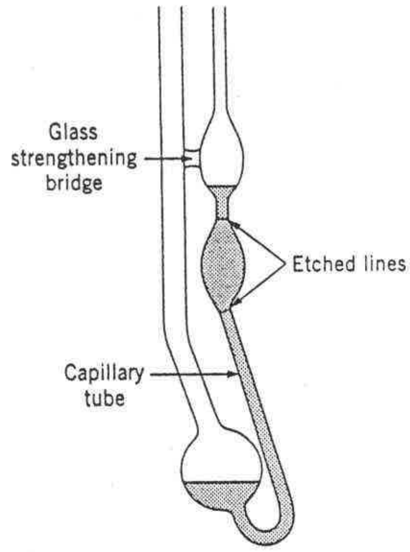
From Fig. B.1 in Appendix B:

$$\mu\,(\text{mercury at } 75°F\,(23.9°C)) \approx 1.5\times10^{-3}\ \frac{N\cdot s}{m^2}$$

$$\mu \approx \left(1.5\times10^{-3}\ \frac{N\cdot s}{m^2}\right)\left(2.089\times10^{-2}\ \frac{\frac{lb\cdot s}{ft^2}}{\frac{N\cdot s}{m^2}}\right) \approx 3.1\times10^{-5}\ \frac{lb\cdot s}{ft^2}$$

1.58

1.58 One type of *capillary-tube viscometer* is shown in **Video V1.5** and in Fig. P1.58. For this device the liquid to be tested is drawn into the tube to a level above the top etched line. The time is then obtained for the liquid to drain to the bottom etched line. The kinematic viscosity, ν, in m^2/s is then obtained from the equation $\nu = KR^4t$ where K is a constant, R is the radius of the capillary tube in mm, and t is the drain time in seconds. When glycerin at 20°C is used as a calibration fluid in a particular viscometer the drain time is 1,430 s. When a liquid having a density of 970 kg/m^3 is tested in the same viscometer the drain time is 900 s. What is the dynamic viscosity of this liquid?



■ FIGURE P1.58

$$\nu = KR^4t$$

For glycerin @ 20°C $\nu = 1.19\times10^{-3}\ m^2/s$

$$\therefore\ 1.19\times10^{-3}\ m^2/s = (KR^4)(1{,}430\ s)$$

$$KR^4 = 8.32\times10^{-7}\ m^2/s^2$$

For unknown liquid with $t = 900 s$

$$\nu = (8.32\times10^{-7}\ m^2/s^2)(900\ s)$$

$$= 7.49\times10^{-4}\ m^2/s$$

Since $\mu = \rho\nu$

$$= (970\ kg/m^3)(7.49\times10^{-4}\ m^2/s)$$

$$= 0.727\ \frac{kg}{m\cdot s} = \underline{\underline{0.727\ \frac{N\cdot s}{m^2}}}$$

1.59

1.59 The viscosity of a soft drink was determined by using a capillary tube viscometer similar to that shown in Fig. P1.47 and Video V1.5. For this device the kinematic viscosity, ν, is directly proportional to the time, t, that it takes for a given amount of liquid to flow through a small capillary tube. That is, $\nu = Kt$. The following data were obtained from regular pop and diet pop. The corresponding measured specific gravities are also given. Based on these data, by what percent is the absolute viscosity, μ, of regular pop greater than that of diet pop?

	Regular pop	Diet pop
t(s)	377.8	300.3
SG	1.044	1.003

$$\% \text{ greater} = \left[\frac{\mu_{reg} - \mu_{diet}}{\mu_{diet}}\right] \times 100 = \left[\frac{\mu_{reg}}{\mu_{diet}} - 1\right] \times 100$$

Since $\nu = \mu/\rho$, $\nu = kt$, and $\rho = (SG)\rho_{H_2O @ 4°C}$

it follows that

$$\% \text{ greater} = \left[\frac{(\nu\rho)_{reg}}{(\nu\rho)_{diet}} - 1\right] \times 100$$

$$= \left[\frac{(t \times SG)_{reg}}{(t \times SG)_{diet}} - 1\right] \times 100$$

$$= \left[\frac{(377.8\text{ s})(1.044)}{(300.3\text{ s})(1.003)} - 1\right] \times 100$$

$$= \underline{\underline{31.0\%}}$$

1.60

1.60 Determine the ratio of the dynamic viscosity of water to air at a temperature of 60 °C. Compare this value with the corresponding ratio of kinematic viscosities. Assume the air is at standard atmospheric pressure.

From Table B.2 in Appendix B:

(for water at 60°C) $\mu = 4.665 \times 10^{-4} \frac{N \cdot s}{m^2}$; $\nu = 4.745 \times 10^{-7} \frac{m^2}{s}$

From Table B.4 in Appendix B:

(for air at 60°C) $\mu = 1.97 \times 10^{-5} \frac{N \cdot s}{m^2}$; $\nu = 1.86 \times 10^{-5} \frac{m^2}{s}$

Thus,

$$\frac{\mu_{H_2O}}{\mu_{air}} = \frac{4.665 \times 10^{-4}}{1.97 \times 10^{-5}} = \underline{\underline{23.7}}$$

$$\frac{\nu_{H_2O}}{\nu_{air}} = \frac{4.745 \times 10^{-7}}{1.86 \times 10^{-5}} = \underline{\underline{2.55 \times 10^{-2}}}$$

1.61

1.61 The viscosity of a certain fluid is 5×10^{-4} poise. Determine its viscosity in both SI and BG units.

From Appendix E, $10^{-1}\ \frac{N \cdot s}{m^2} = 1$ poise. Thus,

$$\mu = (5 \times 10^{-4}\ \text{poise})\left(10^{-1}\ \frac{\frac{N \cdot s}{m^2}}{\text{poise}}\right) = \underline{\underline{5 \times 10^{-5}\ \frac{N \cdot s}{m^2}}}$$

and from Table 1.4

$$\mu = \left(5 \times 10^{-5}\ \frac{N \cdot s}{m^2}\right)\left(2.089 \times 10^{-2}\ \frac{\frac{lb \cdot s}{ft^2}}{\frac{N \cdot s}{m^2}}\right) = \underline{\underline{10.4 \times 10^{-7}\ \frac{lb \cdot s}{ft^2}}}$$

1.62

1.62 The kinematic viscosity and specific gravity of a liquid are $3.5 \times 10^{-4}\ m^2/s$ and 0.79, respectively. What is the dynamic viscosity of the liquid in SI units?

$$\mu = \nu \rho$$

$$\rho = (SG)(\rho_{H_2O @ 4°C})$$

$$\mu = \left(3.5 \times 10^{-4}\ \frac{m^2}{s}\right)\left(0.79 \times 10^3\ \frac{kg}{m^3}\right) = 0.277\ \frac{kg}{m \cdot s} = \underline{\underline{0.277\ \frac{N \cdot s}{m^2}}}$$

1.63

1.63 A liquid has a specific weight of 59 lb/ft^3 and a dynamic viscosity of 2.75 lb·s/ft^2. Determine its kinematic viscosity.

Since $\nu = \frac{\mu}{\rho}$ and $\rho = \frac{\gamma}{g}$,

$$\nu = \frac{\mu g}{\gamma} = \frac{\left(2.75 \frac{lb \cdot s}{ft^2}\right)\left(32.2 \frac{ft}{s^2}\right)}{59 \frac{lb}{ft^3}} = \underline{\underline{1.50 \frac{ft^2}{s}}}$$

1.64

1.64 The kinematic viscosity of oxygen at 20 °C and a pressure of 150 kPa (abs) is 0.104 stokes. Determine the dynamic viscosity of oxygen at this temperature and pressure.

$$\mu = \nu \rho$$

$$\rho = \frac{p}{RT} = \frac{150 \times 10^3 \frac{N}{m^2}}{\left(259.8 \frac{J}{kg \cdot K}\right)\left[(20^\circ C + 273)K\right]} = 1.97 \frac{kg}{m^3}$$

$$\nu = 0.104 \text{ stokes} = 0.104 \frac{cm^2}{s}$$

$$\mu = \left(0.104 \frac{cm^2}{s}\right)\left(10^{-4} \frac{m^2}{cm^2}\right)\left(1.97 \frac{kg}{m^3}\right)$$

$$= 2.05 \times 10^{-5} \frac{kg}{m \cdot s} = \underline{\underline{2.05 \times 10^{-5} \frac{N \cdot s}{m^2}}}$$

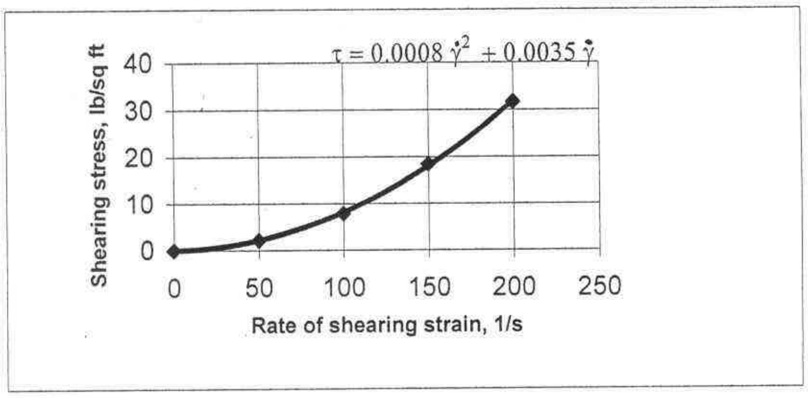
*1.65

*1.65 Fluids for which the shearing stress, τ, is not linearly related to the rate of shearing strain, $\dot{\gamma}$, are designated as non-Newtonian fluids. Such fluids are commonplace and can exhibit unusual behavior as shown in Video V1.6. Some experimental data obtained for a particular non-Newtonian fluid at 80 °F are shown below.

τ (lb/ft^2)	0	2.11	7.82	18.5	31.7
$\dot{\gamma}$ (s^{-1})	0	50	100	150	200

Plot these data and fit a second-order polynomial to the data using a suitable graphing program. What is the apparent viscosity of this fluid when the rate of shearing strain is 70 s^{-1}? Is this apparent viscosity larger or smaller than that for water at the same temperature?

Rate of shearing strain, 1/s	Shearing stress, lb/sq ft
0	0
50	2.11
100	7.82
150	18.5
200	31.7



From the graph $\tau = 0.0008\,\dot{\gamma}^2 + 0.0035\,\dot{\gamma}$ where τ is the shearing stress in lb/ft^2 and $\dot{\gamma}$ is the rate of shearing strain in s^{-1}.

$$\mu_{apparent} = \frac{d\tau}{d\dot{\gamma}} = (2)(0.0008)\dot{\gamma} + 0.0035$$

At $\dot{\gamma} = 70\ s^{-1}$

$$\mu_{apparent} = (2)\left(0.0008\ \frac{lb\cdot s^2}{ft^2}\right)(70\ s^{-1}) + 0.0035\ \frac{lb\cdot s}{ft^2}$$

$$= \underline{\underline{0.116\ \frac{lb\cdot s}{ft^2}}}$$

From Table B.1 in Appendix B, $\mu_{H_2O\,@\,80°F} = 1.791 \times 10^{-5}\ \frac{lb\cdot s}{ft^2}$, and since water is a Newtonian fluid this value is independent of $\dot{\gamma}$. Thus, the unknown non-Newtonian fluid has a much <u>larger</u> value.

1.66

1.66 Water flows near a flat surface and some measurements of the water velocity, u, parallel to the surface, at different heights, y, above the surface are obtained. At the surface $y = 0$. After an analysis of the data, the lab technician reports that the velocity distribution in the range $0 < y < 0.1$ ft is given by the equation

$$u = 0.81 + 9.2y + 4.1 \times 10^3 y^3$$

with u in ft/s when y is in ft. (**a**) Do you think that this equation would be valid in any system of units? Explain. (**b**) Do you think this equation is correct? Explain. You may want to look at Video 1.4 to help you arrive at your answer.

(a) $$u = 0.81 + 9.2y + 4.1 \times 10^3 y^3$$

$$[LT^{-1}] \doteq [0.81] + [9.2][L] + [4.1 \times 10^3][L^3]$$

Each term in the equation must have the same dimensions. Thus, the constant 0.81 must have dimensions of LT^{-1}, 9.2 dimensions of T^{-1}, and 4.1×10^3 dimensions of $L^{-2}T^{-1}$. Since the constants in the equation have dimensions their values will change with a change in units. No.

(b) Equation cannot be correct since at $y=0$ $u = 0.81$ ft/s, a non-zero value which would violate the "no-slip" condition. Not correct.

1.67

1.67 Calculate the Reynolds numbers for the flow of water and for air through a 4-mm-diameter tube, if the mean velocity is 3 m/s and the temperature is 30 °C in both cases (see Example 1.4). Assume the air is at standard atmospheric pressure.

For water at 30°C (from Table B.2 in Appendix B):

$$\rho = 995.7 \ \frac{kg}{m^3} \qquad \mu = 7.975 \times 10^{-4} \ \frac{N \cdot s}{m^2}$$

$$Re = \frac{\rho V D}{\mu} = \frac{\left(995.7 \frac{kg}{m^3}\right)\left(3 \frac{m}{s}\right)(0.004 \ m)}{7.975 \times 10^{-4} \ \frac{N \cdot s}{m^2}} = \underline{\underline{15{,}000}}$$

For air at 30°C (from Table B.4 in Appendix B):

$$\rho = 1.165 \ \frac{kg}{m^3} \qquad \mu = 1.86 \times 10^{-5} \ \frac{N \cdot s}{m^2}$$

$$Re = \frac{\rho V D}{\mu} = \frac{\left(1.165 \frac{kg}{m^3}\right)\left(3 \frac{m}{s}\right)(0.004 \ m)}{1.86 \times 10^{-5} \ \frac{N \cdot s}{m^2}} = \underline{\underline{752}}$$

1.68

1.68 SAE 30 oil at 60 °F flows through a 2-in.-diameter pipe with a mean velocity of 5 ft/s. Determine the value of the Reynolds number (see Example 1.4).

$\rho = 1.77 \ \frac{slugs}{ft^3} \qquad \mu = 8.0 \times 10^{-3} \ \frac{lb \cdot s}{ft^2}$

$$Re = \frac{\rho V D}{\mu} = \frac{\left(1.77 \ \frac{slugs}{ft^3}\right)\left(5 \ \frac{ft}{s}\right)\left(\frac{2}{12} \ ft\right)}{8.0 \times 10^{-3} \ \frac{lb \cdot s}{ft^2}} = \underline{\underline{184}}$$

1,49

1.69

1.69 For air at standard atmospheric pressure the values of the constants that appear in the Sutherland equation (Eq. 1.10) are $C = 1.458 \times 10^{-6}$ kg/(m·s·$K^{1/2}$) and $S = 110.4$ K. Use these values to predict the viscosity of air at 10 °C and 90 °C and compare with values given in Table B.4 in Appendix B.

$$\mu = \frac{C T^{\frac{3}{2}}}{T + S} = \frac{\left(1.458 \times 10^{-6} \frac{kg}{m \cdot s \cdot K^{1/2}}\right) T^{\frac{3}{2}}}{T + 110.4\ K}$$

For $T = 10°C = 10°C + 273.15 = 283.15\ K$,

$$\mu = \frac{(1.458 \times 10^{-6})(283.15\ K)^{3/2}}{283.15\ K + 110.4} = \underline{\underline{1.765 \times 10^{-5} \frac{N \cdot s}{m^2}}}$$

From Table B.4, $\mu = 1.76 \times 10^{-5} \frac{N \cdot s}{m^2}$

For $T = 90°C = 90°C + 273.15 = 363.15\ K$,

$$\mu = \frac{(1.458 \times 10^{-6})(363.15\ K)^{3/2}}{363.15\ K + 110.4} = \underline{\underline{2.13 \times 10^{-5} \frac{N \cdot s}{m^2}}}$$

From Table B.4, $\mu = 2.14 \times 10^{-5} \frac{N \cdot s}{m^2}$

1.50

1.70 *

1.70* Use the values of viscosity of air given in Table B.4 at temperatures of 0, 20, 40, 60, 80, and 100 °C to determine the constants C and S which appear in the Sutherland equation (Eq. 1.10). Compare your results with the values given in Problem 1. (*Hint*: Rewrite the equation in the form

$$\frac{T^{3/2}}{\mu} = \left(\frac{1}{C}\right)T + \frac{S}{C}$$

and plot $T^{3/2}/\mu$ versus T. From the slope and intercept of this curve C and S can be obtained.)

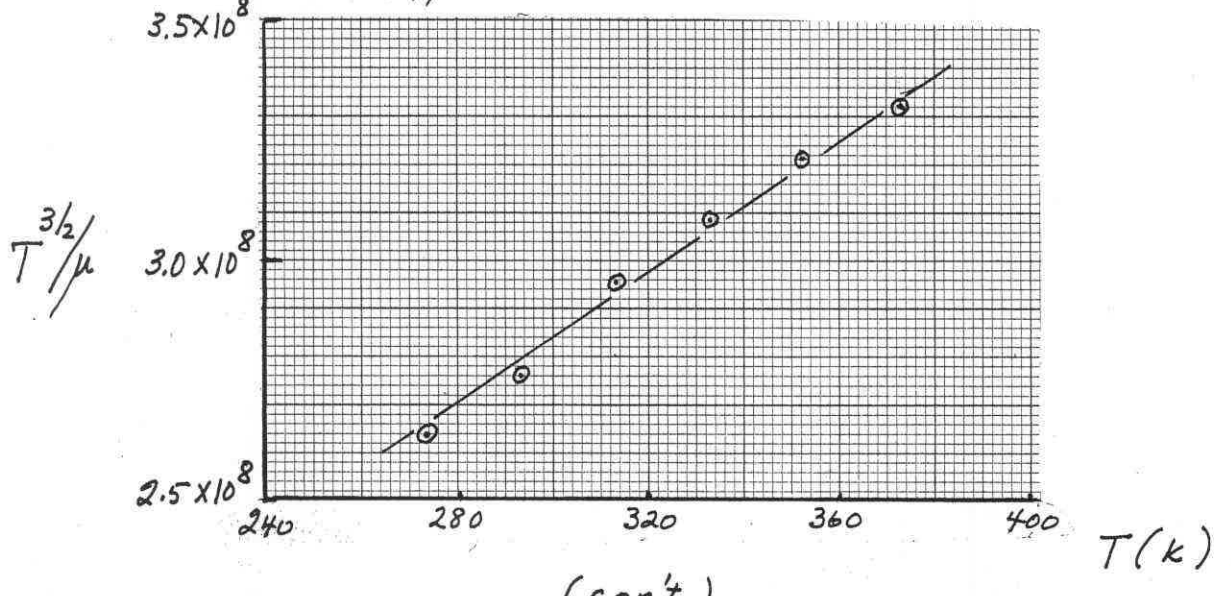
Equation 1.10 can be written in the form

$$\frac{T^{3/2}}{\mu} = \left(\frac{1}{C}\right)T + \frac{S}{C} \qquad (1)$$

and with the data from Table B.4:

$T(°C)$	$T(K)$	$\mu\ (N\cdot s/m^2)$	$T^{3/2}/\mu\ [K^{3/2}/(kg/m\cdot s)]$
0	273.15	1.71×10^{-5}	2.640×10^{8}
20	293.15	1.82×10^{-5}	2.758×10^{8}
40	313.15	1.87×10^{-5}	2.963×10^{8}
60	333.15	1.97×10^{-5}	3.087×10^{8}
80	353.15	2.07×10^{-5}	3.206×10^{8}
100	373.15	2.17×10^{-5}	3.322×10^{8}

A plot of $T^{3/2}/\mu$ vs. T is shown below:



(con't)

1.70 * (Con't)

Since the data plot as an approximate straight line, Eq. (1) can be represented by an equation of the form

$$y = bx + a$$

where $y \sim T^{3/2}/\mu$, $x \sim T$, $b \sim 1/C$, and $a \sim S/C$.

Fit the data to a linear equation using a standard curve-fitting program such as found in EXCEL. Thus,

$$y = 6.969 \times 10^5 x + 7.441 \times 10^7$$

and

$$\frac{1}{C} = b = 6.969 \times 10^5$$

so that

$$\underline{\underline{C = 1.43 \times 10^{-6} \ kg/(m \cdot s \cdot K^{1/2})}}$$

and

$$\frac{S}{C} = a = 7.441 \times 10^7$$

and therefore

$$\underline{\underline{S = 107 \ K}}$$

These values for C and S are in good agreement with values given in Problem 1.69.

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1.71

1.71 The viscosity of a fluid plays a very important role in determining how a fluid flows. (See Video V1.3) The value of the viscosity depends not only on the specific fluid but also on the fluid temperature. Some experiments show that when a liquid, under the action of a constant driving pressure, is forced with a low velocity, V, through a small horizontal tube, the velocity is given by the equation $V = K/\mu$. In this equation K is a constant for a given tube and pressure, and μ is the dynamic viscosity. For a particular liquid of interest, the viscosity is given by Andrade's equation (Eq. 1.11) with $D = 5 \times 10^{-7}\ \text{lb} \cdot \text{s/ft}^2$ and $B = 4000\ °R$. By what percentage will the velocity increase as the liquid temperature is increased from 40 °F to 100 °F? Assume all other factors remain constant.

$$V_{40°} = \frac{K}{\mu_{40°}} \qquad (1)$$

$$V_{100°} = \frac{K}{\mu_{100°}} \qquad (2)$$

$$\%\ \text{increase in } V = \left[\frac{V_{100°} - V_{40°}}{V_{40°}}\right] \times 100 = \left[\frac{V_{100°}}{V_{40°}} - 1\right] \times 100$$

and from Eq. (1) & (2)

$$\%\ \text{increase in } V = \left[\frac{K/\mu_{100°}}{K/\mu_{40°}} - 1\right] \times 100 = \left[\frac{\mu_{40°}}{\mu_{100°}} - 1\right] \times 100 \qquad (3)$$

From Andrade's equation

$$\mu_{40°} = 5 \times 10^{-7}\, e^{\frac{4000}{(40°F + 460)}}$$

and

$$\mu_{100°} = 5 \times 10^{-7}\, e^{\frac{4000}{(100°F + 460)}}$$

Thus, from Eq. (3)

$$\%\ \text{increase in } V = \left[\frac{5 \times 10^{-7}\, e^{\frac{4000}{500}}}{5 \times 10^{-7}\, e^{\frac{4000}{560}}} - 1\right] \times 100$$

$$= \underline{\underline{136\%}}$$

1.52

*1.72

***1.72** Use the value of the viscosity of water given in Table B.2 at temperatures of 0, 20, 40, 60, 80, and 100 °C to determine the constants D and B which appear in Andrade's equation (Eq. 1.11). Calculate the value of the viscosity at 50 °C and compare with the value given in Table B.2. (*Hint*: Rewrite the equation in the form

$$\ln \mu = (B)\frac{1}{T} + \ln D$$

and plot ln μ versus $1/T$. From the slope and intercept of this curve B and D can be obtained. If a nonlinear curve fitting program is available the constants can be obtained directly from Eq. 1.11 without rewriting the equation.)

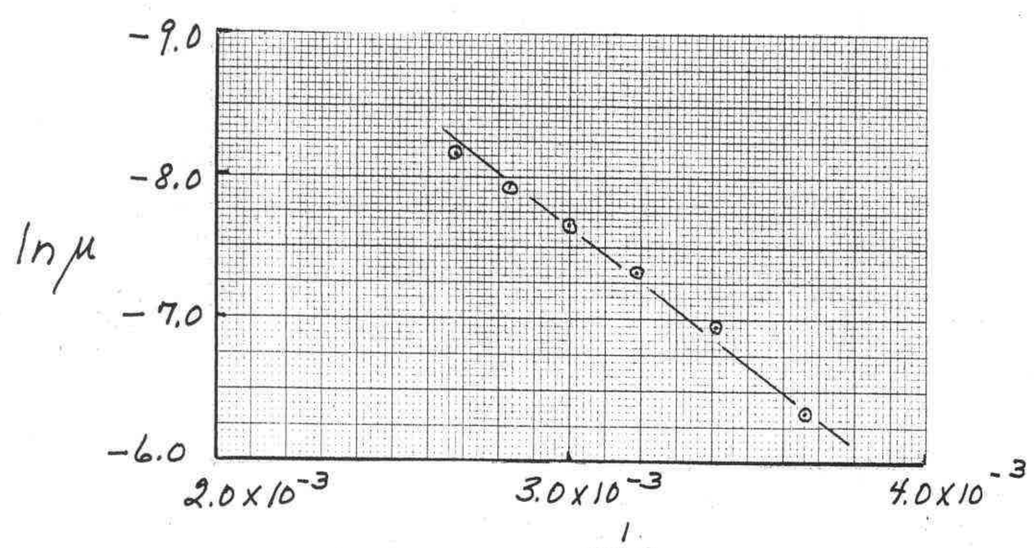
Equation 1.11 can be written in the form

$$\ln \mu = (B)\frac{1}{T} + \ln D \qquad (1)$$

and with the data from Table B.2:

T (°C)	T (K)	$1/T$ (K)	μ (N·s/m²)	ln μ
0	273.15	3.661×10^{-3}	1.787×10^{-3}	−6.327
20	293.15	3.411×10^{-3}	1.002×10^{-3}	−6.906
40	313.15	3.193×10^{-3}	6.529×10^{-4}	−7.334
60	333.15	3.002×10^{-3}	4.665×10^{-4}	−7.670
80	353.15	2.832×10^{-3}	3.547×10^{-4}	−7.944
100	373.15	2.680×10^{-3}	2.818×10^{-4}	−8.174

A plot of ln μ vs. $1/T$ is shown below:



(con't)

*1.72 (con't)

Since the data plot as an approximate straight line, Eq. (1) can be used to represent these data. To obtain B and D, fit the data to an exponential equation of the form $y = ae^{bx}$ such as found in EXCEL.

Thus,

$$\underline{\underline{D = a = 1.767 \times 10^{-6} \ N \cdot s/m^2}}$$

and

$$\underline{\underline{B = b = 1.870 \times 10^{3} \ K}}$$

so that

$$\mu = 1.767 \times 10^{-6} \, e^{\frac{1870}{T}}$$

At 50°C (323.15K),

$$\mu = 1.767 \times 10^{-6} \, e^{\frac{1870}{323.15}} = \underline{\underline{5.76 \times 10^{-4} \ N \cdot s/m^2}}$$

From Table B.2, $\mu = 5.468 \times 10^{-4} \ N \cdot s/m^2$.

1.73

1.73 For a certain liquid $\mu = 7.1 \times 10^{-5}$ lb·s/ft^2 at 40 °F and $\mu = 1.9 \times 10^{-5}$ lb·s/ft^2 at 150 °F. Make use of these data to determine the constants D and B which appear in Andrade's equation (Eq. 1.11). What would be the viscosity at 80 °F?

$$\mu = D e^{\frac{B}{T}} \qquad \text{(Eq. 1.11)}$$

At $T = (40°F + 459.67) = 499.67\,°R$, $\mu = 7.1 \times 10^{-5}\ \frac{lb \cdot s}{ft^2}$,
and
at $T = (150°F + 459.67) = 609.67\,°R$, $\mu = 1.9 \times 10^{-5}\ \frac{lb \cdot s}{ft^2}$.

Take the logarithm of both sides of Eq. 1.11 to yield

$$\ln \mu = B\left(\frac{1}{T}\right) + \ln D \qquad (1)$$

Substitute above values of μ and T into Eq.(1) to give

$$\ln(7.1 \times 10^{-5}) = B\left(\frac{1}{499.67}\right) + \ln D \qquad (2)$$

$$\ln(1.9 \times 10^{-5}) = B\left(\frac{1}{609.67}\right) + \ln D \qquad (3)$$

and solve Eqs.(2) and (3) simultaneously for B and D.
Subtract Eq.(3) from Eq.(2) to give

$$\ln\left(\frac{7.1 \times 10^{-5}}{1.9 \times 10^{-5}}\right) = B\left(\frac{1}{499.67} - \frac{1}{609.67}\right)$$

and $\therefore B = 3650$. Substitute this value of B into Eq. (2) to yield

$$\ln(7.1 \times 10^{-5}) = 3650\left(\frac{1}{499.67}\right) + \ln D$$

and $\therefore D = 4.77 \times 10^{-8}$. Thus,

$$\underline{\underline{B = 3650}} \quad \text{and} \quad \underline{\underline{D = 4.77 \times 10^{-8}}}$$

At $T = 80°F + 459.67 = 539.67\,°R$

$$\mu = 4.77 \times 10^{-8}\, e^{\frac{3650}{539.67}} = \underline{\underline{4.13 \times 10^{-5}\ \frac{lb \cdot s}{ft^2}}}$$

1.74

1.74 For a parallel plate arrangement of the type shown in Fig. 1.5 it is found that when the distance between plates is 2 mm, a shearing stress of 150 Pa develops at the upper plate when it is pulled at a velocity of 1 m/s. Determine the viscosity of the fluid between the plates. Express your answer in SI units.

$$\tau = \mu \frac{du}{dy}$$

$$\frac{du}{dy} = \frac{U}{b}$$

$$\mu = \frac{\tau}{\left(\frac{U}{b}\right)} = \frac{150 \frac{N}{m^2}}{\left(\frac{1 \frac{m}{s}}{0.002 m}\right)} = \underline{\underline{0.300 \frac{N \cdot s}{m^2}}}$$

1.75

1.75 Two flat plates are oriented parallel above a fixed lower plate as shown in Fig. P1.75. The top plate, located a distance b above the fixed plate, is pulled along with speed V. The other thin plate is located a distance cb, where $0 < c < 1$, above the fixed plate. This plate moves with speed V_1, which is determined by the viscous shear forces imposed on it by the fluids on its top and bottom. The fluid on the top is twice as viscous as that on the bottom. Plot the ratio V_1/V as a function of c for $0 < c < 1$.

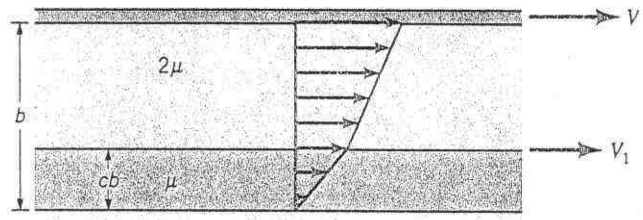


FIGURE P1.75

For constant speed, V_1, of the middle plate, the net force on the plate is 0. Hence, $F_{top} = F_{bottom}$, where $F = \tau A$. Thus, the shear stress on the top and bottom of the plate must be equal.

$$\tau_{top} = \tau_{bottom} \quad \text{where} \quad \tau = \mu \frac{du}{dy} \qquad (1)$$

For the bottom fluid $\frac{du}{dy} = \frac{V_1}{cb}$, while for the top fluid $\frac{du}{dy} = \frac{(V-V_1)}{b-cb}$

Hence, from Eqn. (1),

$$(2\mu)\frac{(V-V_1)}{b(1-c)} = (\mu)\frac{V_1}{cb}$$, which can be written as:

$$2cV - 2cV_1 = V_1 - cV_1$$

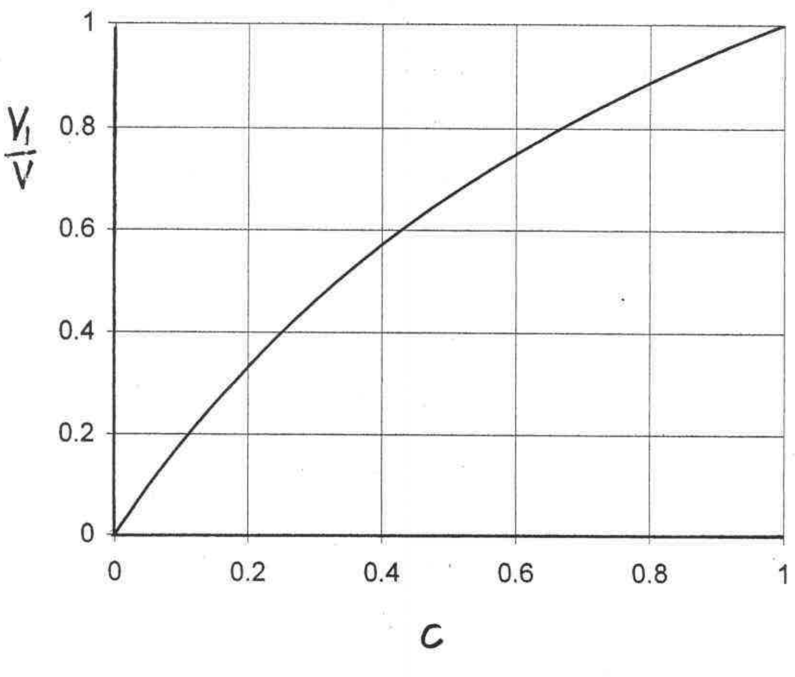
or

$$\frac{V_1}{V} = \frac{2c}{c+1}$$

Note: If $c = 0$, $\frac{V_1}{V} = 0$

If $c = \frac{1}{2}$, $\frac{V_1}{V} = \frac{2}{3}$

If $c = 1$, $\frac{V_1}{V} = 1$



1.76

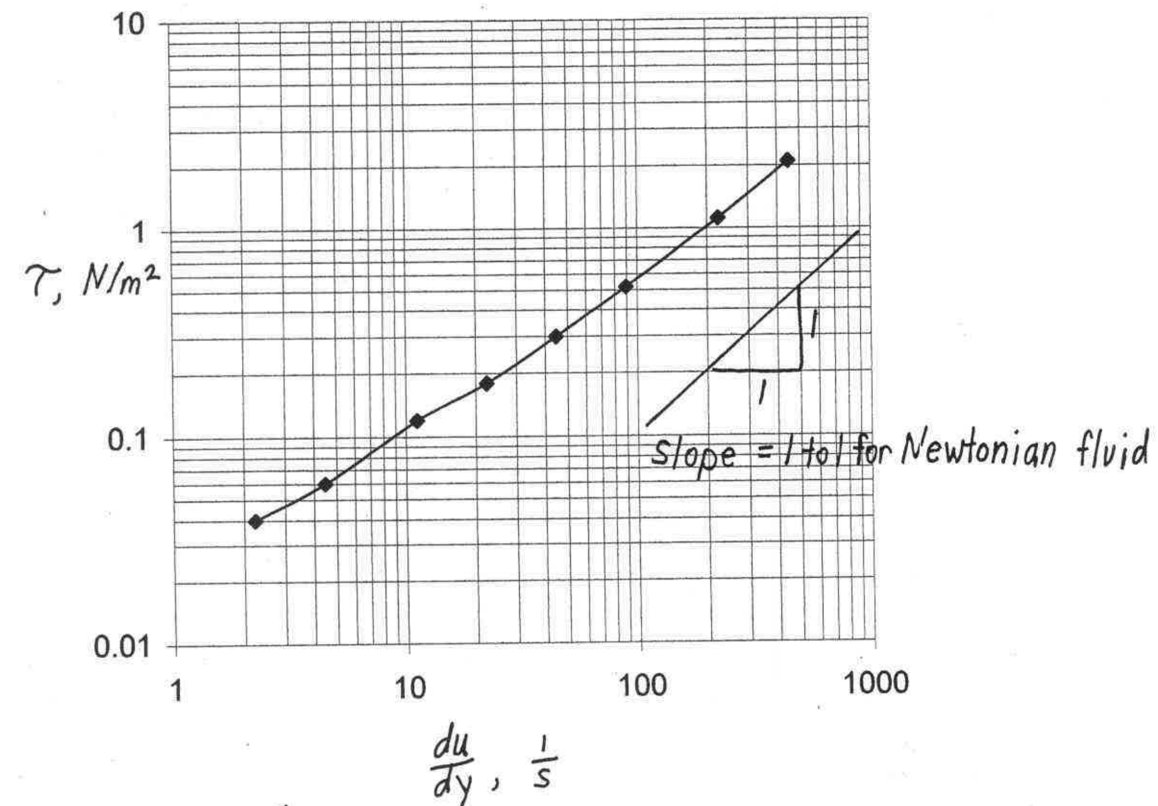
1.76 There are many fluids that exhibit non-Newtonian behavior (see, for example, Video V1.6). For a given fluid the distinction between Newtonian and non-Newtonian behavior is usually based on measurements of shear stress and rate of shearing strain. Assume that the viscosity of blood is to be determined by measurements of shear stress, τ, and rate of shearing strain, du/dy, obtained from a small blood sample tested in a suitable viscometer. Based on the data given below determine if the blood is a Newtonian or non-Newtonian fluid. Explain how you arrived at your answer.

τ (N/m^2)	0.04	0.06	0.12	0.18	0.30	0.52	1.12	2.10
du/dy (s^{-1})	2.25	4.50	11.25	22.5	45.0	90.0	225	450

For a Newtonian fluid the ratio of τ to du/dy is a constant. For the data given:

$\frac{\tau}{du/dy}$ ($N \cdot s/m^2$)	0.0178	0.0133	0.0107	0.0080	0.0067	0.0058	0.0050	0.0047

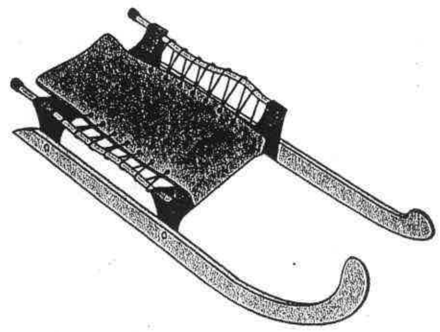
The ratio is not a constant but decreases as the rate of shearing strain increases. Thus, this fluid (blood) is a non-Newtonian fluid. A plot of the data is shown below. For a Newtonian fluid the curve would be a straight line with a slope of 1 to 1.



Note: $\tau = \mu \left(\frac{du}{dy}\right)^a$, where $a = 1$ for a Newtonian fluid.

1.77

1.77 The sled shown in Fig. P1.77 slides along on a thin horizontal layer of water between the ice and the runners. The horizontal force that the water puts on the runners is equal to 1.2 lb when the sled's speed is 50 ft/s. The total area of both runners in contact with the water is 0.08 ft^2, and the viscosity of the water is 3.5×10^{-5} lb s/ft^2. Determine the thickness of the water layer under the runners. Assume a linear velocity distribution in the water layer.



■ FIGURE P1.77

F (force) $= \tau A$

$\tau = \mu \frac{dv}{dy} = \mu \frac{V}{d}$ where d = thickness of water layer

Thus,

$$F = \mu \frac{V}{d} A$$

and

$$d = \frac{\mu V A}{F} = \frac{\left(3.5\times10^{-5}\ \frac{lb\cdot s}{ft^2}\right)\left(50\ \frac{ft}{s}\right)\left(0.08\ ft^2\right)}{1.2\ lb}$$

$$= \underline{\underline{11.7\times10^{-4}\ ft}}$$

1.78

1.78 A 25-mm-diameter shaft is pulled through a cylindrical bearing as shown in Fig. P1.78 The lubricant that fills the 0.3-mm gap between the shaft and bearing is an oil having a kinematic viscosity of $8.0 \times 10^{-4}\ m^2/s$ and a specific gravity of 0.91. Determine the force P required to pull the shaft at a velocity of 3 m/s. Assume the velocity distribution in the gap is linear.

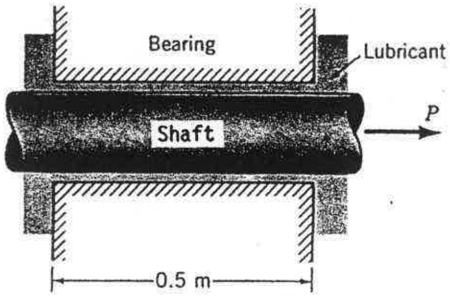
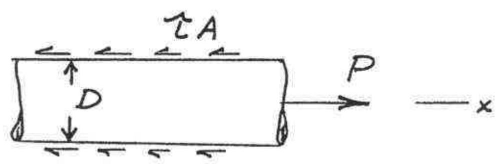


FIGURE P1.78



$$\sum F_x = 0$$

Thus, $P = \tau A$

where $A = \pi D \times (\text{shaft length in bearing}) = \pi D \ell$

and $\tau = \mu \dfrac{(\text{velocity of shaft})}{(\text{gap width})} = \mu \dfrac{V}{b}$

so that

$$P = \left(\mu \frac{V}{b}\right)(\pi D \ell)$$

Since $\mu = \nu \rho = \nu (SG)(\rho_{H_2O @ 4°C})$,

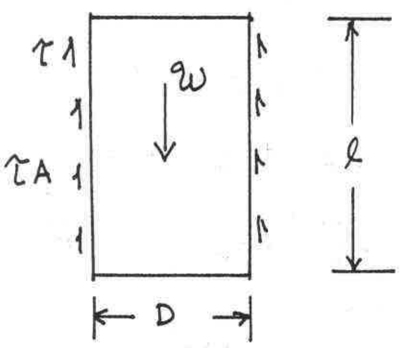
$$P = \frac{(8.0 \times 10^{-4} \frac{m^2}{s})(0.91 \times 10^3 \frac{kg}{m^3})(3 \frac{m}{s})(\pi)(0.025m)(0.5m)}{(0.0003m)}$$

$$= \underline{\underline{286\ N}}$$

1.79

1.79 A piston having a diameter of 5.48 in. and a length of 9.50 in. slides downward with a velocity V through a vertical pipe. The downward motion is resisted by an oil film between the piston and the pipe wall. The film thickness is 0.002 in., and the cylinder weighs 0.5 lb. Estimate V if the oil viscosity is 0.016 lb·s/ft². Assume the velocity distribution in the gap is linear.

$$\Sigma F_{vertical} = 0$$



Thus, $\mathcal{W} = \tau A$

where $A = \pi D \ell$

and $\tau = \mu \dfrac{(\text{velocity})}{(\text{film thickness})} = \mu \dfrac{V}{\delta}$

so that

$$\mathcal{W} = \left(\mu \frac{V}{\delta}\right)(\pi D \ell)$$

It follows that

$$V = \frac{\mathcal{W}\delta}{\pi D \ell \mu} = \frac{(0.5\,\text{lb})\left(\frac{0.002}{12}\,\text{ft}\right)}{\pi\left(\frac{5.48}{12}\,\text{ft}\right)\left(\frac{9.50}{12}\,\text{ft}\right)\left(0.016\,\frac{\text{lb}\cdot\text{s}}{\text{ft}^2}\right)}$$

$$= \underline{\underline{0.00459\ \frac{\text{ft}}{\text{s}}}}$$

1.80

1.80 A 10-kg block slides down a smooth inclined surface as shown in Fig. P1.80. Determine the terminal velocity of the block if the 0.1-mm gap between the block and the surface contains SAE 30 oil at 60 °F. Assume the velocity distribution in the gap is linear, and the area of the block in contact with the oil is 0.1 m².

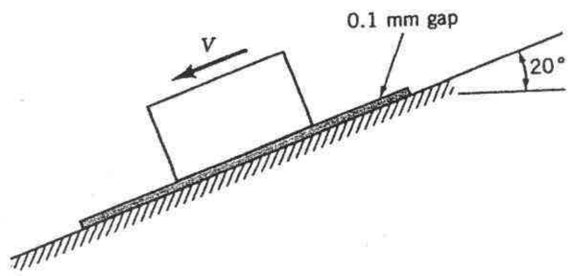
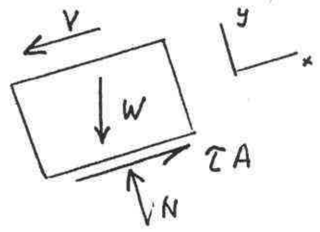


FIGURE P1.80



$$\sum F_x = 0$$

Thus,

$$W \sin 20° = \tau A$$

Since

$$\tau = \mu \frac{V}{b}$$, where b is film thickness,

$$W \sin 20° = \mu \frac{V}{b} A$$

Thus, (with $W = mg$)

$$V = \frac{b W \sin 20°}{\mu A} = \frac{(0.0001\,m)(10\,kg)(9.81\,\frac{m}{s^2})(\sin 20°)}{(0.38\,\frac{N \cdot s}{m^2})(0.1\,m^2)}$$

$$= \underline{\underline{0.0883\ \frac{m}{s}}}$$

1.81

1.81 A layer of water flows down an inclined fixed surface with the velocity profile shown in Fig. P1.81. Determine the magnitude and direction of the shearing stress that the water exerts on the fixed surface for $U = 2$ m/s and $h = 0.1$ m.

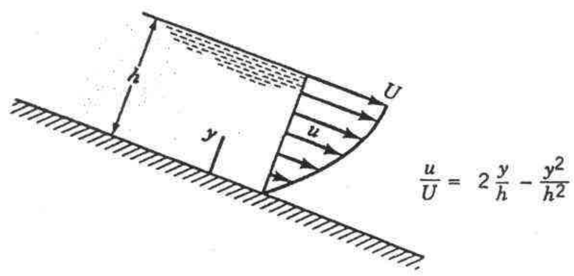


FIGURE P1.81

$$\tau = \mu \frac{du}{dy}$$

$$\frac{du}{dy} = U\left(\frac{2}{h} - \frac{y^2}{h^2}\right)$$

Thus, at the fixed surface $(y=0)$

$$\left(\frac{du}{dy}\right)_{y=0} = \frac{2U}{h}$$

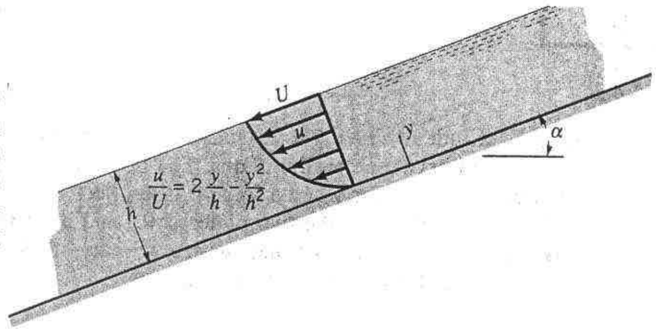
so that

$$\tau = \mu\left(\frac{2U}{h}\right) = \left(1.12\times10^{-3}\ \frac{N\cdot s}{m^2}\right)(2)\ \frac{\left(2\ \frac{m}{s}\right)}{(0.1\,m)}$$

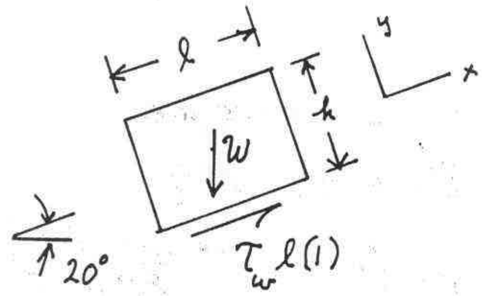
$$= 4.48\times10^{-2}\ \frac{N}{m^2} \quad \text{acting in direction of flow}$$

1.82

1.82 A thin layer of glycerin flows down an inclined, wide plate with the velocity distribution shown in Fig. P1.82. For h = 0.3 in. and α = 20°, determine the surface velocity, U. Note that for equilibrium, the component of weight acting parallel to the plate surface must be balanced by the shearing force developed along the plate surface. In your analysis assume a unit plate width.



■ FIGURE P1.82



$$\Sigma F_x = 0$$

Thus,

$$\mathcal{W} \sin 20° = \tau_w \, \ell (1)$$

and with $\mathcal{W} = \gamma \ell h (1)$

$$\gamma \ell h (1) \sin 20° = \tau_w \, \ell (1)$$

or

$$\gamma h \sin 20° = \tau_w \qquad (1)$$

At the plate

$$\tau_w = \mu \left(\frac{du}{dy} \right)_{y=0}$$

Since

$$\frac{du}{dy} = \frac{2U}{h} - \frac{2Uy}{h^2}$$

$$\left(\frac{du}{dy} \right)_{y=0} = \frac{2U}{h}$$

Thus, from Eq. (1)

$$\gamma h \sin 20° = \mu \frac{2U}{h}$$

and

$$U = \frac{\gamma h^2 \sin 20°}{2\mu}$$

$$= \frac{\left(78.6 \frac{lb}{ft^3}\right)\left(\frac{0.3}{12} ft\right)^2 \sin 20°}{2 \left(3.13 \times 10^{-2} \frac{lb \cdot s}{ft^2}\right)} = \underline{\underline{0.268 \frac{ft}{s}}}$$

*1.83

***1.83** Standard air flows past a flat surface and velocity measurements near the surface indicate the following distribution:

y (ft)	0.005	0.01	0.02	0.04	0.06	0.08
u (ft/s)	0.74	1.51	3.03	6.37	10.21	14.43

The coordinate y is measured normal to the surface and u is the velocity parallel to the surface. **(a)** Assume the velocity distribution is of the form

$$u = C_1 y + C_2 y^3$$

and use a standard curve-fitting technique to determine the constants C_1 and C_2. **(b)** Make use of the results of part (a) to determine the magnitude of the shearing stress at the wall ($y = 0$) and at $y = 0.05$ ft.

(a) Use nonlinear regression program to obtain coefficients C_1 and C_2. The program produces least squares estimates of the parameters of a nonlinear model. For the data given,

$$\underline{\underline{C_1 = 153\ s^{-1}}} \quad \text{and} \quad \underline{\underline{C_2 = 4350\ ft^{-2}s^{-1}}}$$

(b) Since,

$$\tau = \mu \frac{du}{dy}$$

it follows that

$$\tau = \mu\left(C_1 + 3C_2 y^2\right)$$

Thus, at the wall ($y=0$)

$$\tau = \mu C_1 = \left(3.74 \times 10^{-7}\ \frac{lb\cdot s}{ft^2}\right)\left(153\ \frac{1}{s}\right) = \underline{\underline{5.72 \times 10^{-5}\ \frac{lb}{ft^2}}}$$

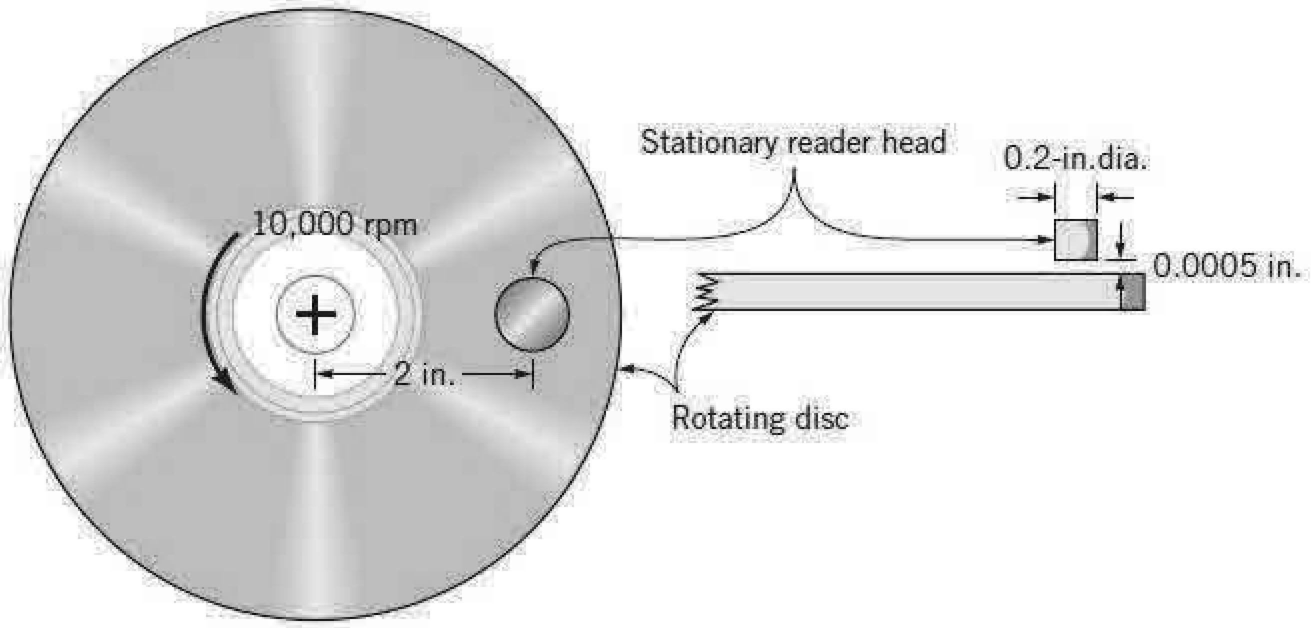
At $y = 0.05$ ft

$$\tau = \left(3.74 \times 10^{-7}\ \frac{lb\cdot s}{ft^2}\right)\left[153\ \frac{1}{s} + 3\left(4350\ \frac{1}{ft^2\cdot s}\right)\left(0.05\ ft\right)^2\right]$$

$$= \underline{\underline{6.94 \times 10^{-5}\ \frac{lb}{ft^2}}}$$

1.84

1.84 A new computer drive is proposed to have a disc, as shown in Fig. P1.84. The disc is to rotate at 10,000 rpm, and the reader head is to be positioned 0.0005 in. above the surface of the disc. Estimate the shearing force on the reader head as result of the air between the disc and the head.



■ Figure P1.84

F = shear force on head = τA, where, if the velocity profile in the gap between the disc and head is linear and uniform across the head, then

$$\tau = \mu \frac{du}{dy} = \mu \frac{U}{b}, \text{ where}$$

$$U = \omega R = 10{,}000 \frac{rev}{min}\left(\frac{1\,min}{60\,s}\right)\left(\frac{2\pi\,rad}{rev}\right)\left(\frac{2}{12}\,ft\right) = 175\,\frac{ft}{s}$$

Thus,

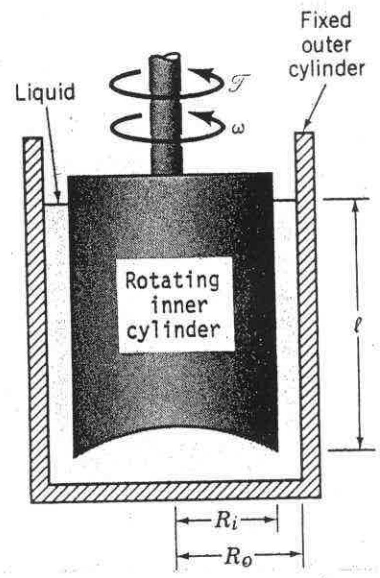
$$\tau = \left(3.74\times10^{-7}\,\frac{lb\cdot s}{ft^2}\right)\frac{175\,\frac{ft}{s}}{\left(\frac{0.0005}{12}\,ft\right)} = 1.57\,\frac{lb}{ft^2}$$

so that

$$F = \tau A = \left(1.57\,\frac{lb}{ft^2}\right)\frac{\pi}{4}\left(\frac{0.2}{12}\,ft\right)^2 = \underline{\underline{3.43\times10^{-4}\,lb}}$$

1.85

1.85 The space between two 6-in.-long concentric cylinders is filled with glycerin (viscosity = 8.5×10^{-3} lb · s/ft²). The inner cylinder has a radius of 3 in. and the gap width between cylinders is 0.1 in. Determine the torque and the power required to rotate the inner cylinder at 180 rev/min. The outer cylinder is fixed. Assume the velocity distribution in the gap to be linear.



Torque, $d\mathcal{T}$, due to shearing stress on inner cylinder is equal to

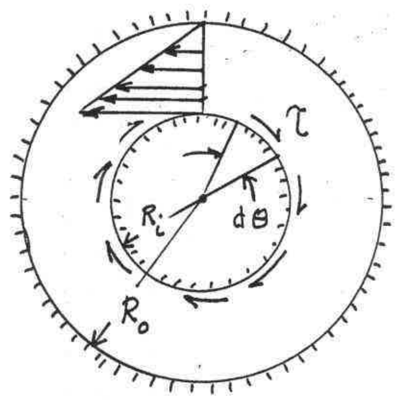
$$d\mathcal{T} = R_i \, \tau \, dA$$

where $dA = (R_i \, d\theta)\,\ell$. Thus,

$$d\mathcal{T} = R_i^2 \, \ell \, \tau \, d\theta$$

and torque required to rotate inner cylinder is

$$\mathcal{T} = R_i^2 \, \ell \, \tau \int_0^{2\pi} d\theta = 2\pi R_i^2 \, \ell \, \tau$$



top view

(ℓ ~ cylinder length)

For a linear velocity distribution in the gap

$$\tau = \mu \frac{R_i \omega}{R_o - R_i} \quad \text{so that}$$

$$\mathcal{T} = \frac{2\pi R_i^3 \, \ell \, \mu \, \omega}{R_o - R_i}$$

and with $\omega = \left(180 \frac{\text{rev}}{\text{min}}\right)\left(2\pi \frac{\text{rad}}{\text{rev}}\right)\left(\frac{1 \text{ min}}{60 \text{ s}}\right) = 6\pi \frac{\text{rad}}{\text{s}}$

then

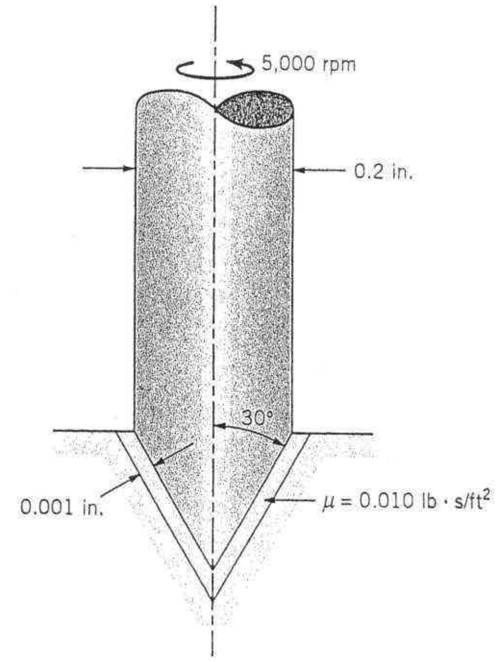
$$\mathcal{T} = \frac{2\pi \left(\frac{3}{12}\text{ft}\right)^3 \left(\frac{6}{12}\text{ft}\right)\left(8.5 \times 10^{-3} \frac{\text{lb}\cdot\text{s}}{\text{ft}^2}\right)\left(6\pi \frac{\text{rad}}{\text{s}}\right)}{\left(\frac{0.1}{12}\text{ft}\right)} = \underline{\underline{0.944 \text{ ft}\cdot\text{lb}}}$$

Since power = $\mathcal{T} \times \omega$ it follows that

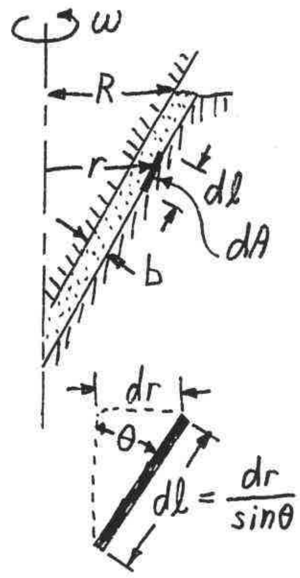
$$\text{power} = (0.944 \text{ ft}\cdot\text{lb})\left(6\pi \frac{\text{rad}}{\text{s}}\right) = \underline{\underline{17.8 \frac{\text{ft}\cdot\text{lb}}{\text{s}}}}$$

1.86

1.86 A pivot bearing used on the shaft of an electrical instrument is shown in Fig. P1.86. An oil with a viscosity of $\mu = 0.010 \text{ lb}\cdot\text{s/ft}^2$ fills the 0.001-in. gap between the rotating shaft and the stationary base. Determine the frictional torque on the shaft when it rotates at 5,000 rpm.



■ FIGURE P1.86



Let $d\mathcal{T}$ = torque on area element dA, where $dA = 2\pi r\, d\ell = 2\pi r\, dr/\sin\theta$

Thus,

$d\mathcal{T} = r\, dF = r\tau\, dA$ where $\tau = \mu \frac{du}{dy} = \mu \frac{\omega r}{b}$

so that,

$$d\mathcal{T} = r\left(\mu \frac{\omega r}{b}\right)(2\pi r\, dr/\sin\theta)$$

$$= \frac{2\pi\mu\omega}{b\sin\theta} r^3 dr$$

Hence,

$$\mathcal{T} = \int d\mathcal{T} = \frac{2\pi\mu\omega}{b\sin\theta}\int_{r=0}^{r=R} r^3 dr = \frac{\pi\mu\omega}{2b\sin\theta}R^4 \qquad (1)$$

Now,

$R = 0.1 \text{ in.}$, $b = 0.001 \text{ in.}$, $\mu = 0.010 \frac{\text{lb}\cdot\text{s}}{\text{ft}^2}$, $\theta = 30\text{deg}$, and

$$\omega = 5{,}000 \frac{\text{rev}}{\text{min}}\left(\frac{\text{min}}{60 \text{ s}}\right)\left(2\pi \frac{\text{rad}}{\text{rev}}\right) = 524 \frac{\text{rad}}{\text{s}}$$

Thus, from Eq. (1),

$$\mathcal{T} = \frac{\pi\left(0.010 \frac{\text{lb}\cdot\text{s}}{\text{ft}^2}\right)\left(524 \frac{\text{rad}}{\text{s}}\right)}{2\left(\frac{0.001}{12}\text{ft}\right)\sin 30^\circ}\left(\frac{0.1}{12}\text{ft}\right)^4 = \underline{\underline{9.53 \times 10^{-4} \text{ ft}\cdot\text{lb}}}$$

56 bi

1.87

1.87 The viscosity of liquids can be measured through the use of a *rotating cylinder viscometer* of the type illustrated in Fig. P1.87. In this device the outer cylinder is fixed and the inner cylinder is rotated with an angular velocity, ω. The torque $\mathcal{T}$ required to develop ω is measured and the viscosity is calculated from these two measurements. (a) Develop an equation relating μ, ω, $\mathcal{T}$, ℓ, R_o, and R_i. Neglect end effects and assume the velocity distribution in the gap is linear. (b) The following torque-angular velocity data were obtained with a rotating cylinder viscometer of the type discussed in part (a).

Torque (ft · lb)	13.1	26.0	39.5	52.7	64.9	78.6
Angular velocity (rad/s)	1.0	2.0	3.0	4.0	5.0	6.0

For this viscometer $R_o = 2.50$ in., $R_i = 2.45$ in., and $\ell = 5.00$ in. Make use of these data and a standard curve-fitting program to determine the viscosity of the liquid contained in the viscometer.

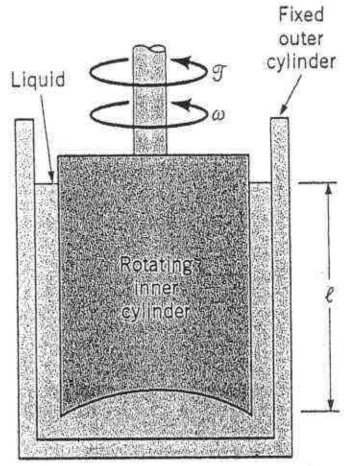


FIGURE P1.87

(a) Torque, $d\mathcal{T}$, due to shearing stress on inner cylinder is equal to

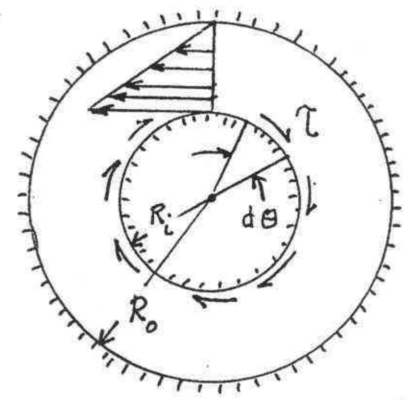
$$d\mathcal{T} = R_i \, \tau \, dA$$

where $dA = (R_i \, d\theta)\ell$. Thus,

$$d\mathcal{T} = R_i^2 \ell \, \tau \, d\theta$$

and torque required to rotate inner cylinder is

$$\mathcal{T} = R_i^2 \ell \, \tau \int_0^{2\pi} d\theta = 2\pi R_i^2 \ell \, \tau$$



top view

(ℓ ~ cylinder length)

For a linear velocity distribution in the gap

$$\tau = \mu \frac{R_i \omega}{R_o - R_i} \quad \text{so that}$$

$$\mathcal{T} = \frac{2\pi R_i^3 \ell \mu \omega}{R_o - R_i} \qquad (1)$$

(b) Thus, for a fixed geometry and a given viscosity, Eq. (1) is of the form

$$y = bx \qquad (y \sim \mathcal{T} \text{ and } x \sim \omega)$$

where b is a constant equal to

(con't)

1.87 (con't)

$$b = \frac{2\pi R_i^3 \ell \mu}{R_o - R_i} \tag{2}$$

To obtain b fit the data to a linear equation of the form $y = bx$ using a standard curve-fitting program such as found in EXCEL.

Thus, from Eq. (2)

$$\mu = \frac{(b)(R_o - R_i)}{2\pi R_i^3 \ell}$$

and with the data given, $b = 13.08 \text{ ft}\cdot\text{lb}\cdot\text{s}$, so that

$$\mu = \frac{(13.08 \text{ ft}\cdot\text{lb}\cdot\text{s})\left(\frac{2.50 - 2.45}{12} \text{ ft}\right)}{2\pi \left(\frac{2.45}{12} \text{ ft}\right)^3 \left(\frac{5.00}{12} \text{ ft}\right)} = \underline{\underline{2.45 \ \frac{\text{lb}\cdot\text{s}}{\text{ft}^2}}}$$

1.88

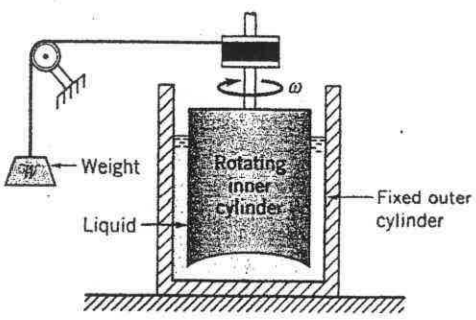
1.88 One type of rotating cylinder viscometer, called a *Stormer* viscometer, uses a falling weight, $\mathcal{W}$, to cause the cylinder to rotate with an angular velocity, ω, as illustrated in Fig. P1.88. For this device the viscosity, μ, of the liquid is related to $\mathcal{W}$ and ω through the equation $\mathcal{W} = K\mu\omega$, where K is a constant that depends only on the geometry (including the liquid depth) of the viscometer. The value of K is usually determined by using a calibration liquid (a liquid of known viscosity).

(a) Some data for a particular Stormer viscometer, obtained using glycerin at 20 °C as a calibration liquid, are given below. Plot values of the weight as ordinates and values of the angular velocity as abscissae. Draw the best curve through the plotted points and determine K for the viscometer.

$\mathcal{W}$ (lb)	0.22	0.66	1.10	1.54	2.20
ω (rev/s)	0.53	1.59	2.79	3.83	5.49

(b) A liquid of unknown viscosity is placed in the same viscometer used in part (a), and the data given below are obtained. Determine the viscosity of this liquid.

$\mathcal{W}$ (lb)	0.04	0.11	0.22	0.33	0.44
ω (rev/s)	0.72	1.89	3.73	5.44	7.42



■ FIGURE P1.88

(a) Since $\mathcal{W} = K\mu\omega$ the slope of the $\mathcal{W}$ vs. ω curve is

$$\text{slope} = K\mu = \frac{\mathcal{W}\,(lb)}{\omega\,(\frac{rev}{s})}$$

so that

$$K = \frac{\text{slope}\,(\frac{lb\cdot s}{rev})}{\mu\,(\frac{lb\cdot s}{ft^2})} \qquad (1)$$

For the glycerin data (see plot on next page) the slope (based on a least squares fit of the data) is

$$\text{slope (glycerin)} = 0.398\ \frac{lb\cdot s}{rev}$$

Since $\mu\,(\text{glycerin}) = 3.13 \times 10^{-2}\ \frac{lb\cdot s}{ft^2}$ then

$$K = \frac{0.398\ \frac{lb\cdot s}{rev}}{3.13\times 10^{-2}\ \frac{lb\cdot s}{ft^2}} = \underline{\underline{12.7\ \frac{ft^2}{rev}}}$$

(b) For the unknown fluid data (see plot on next page) the slope (based on a least squares fit of the data) is

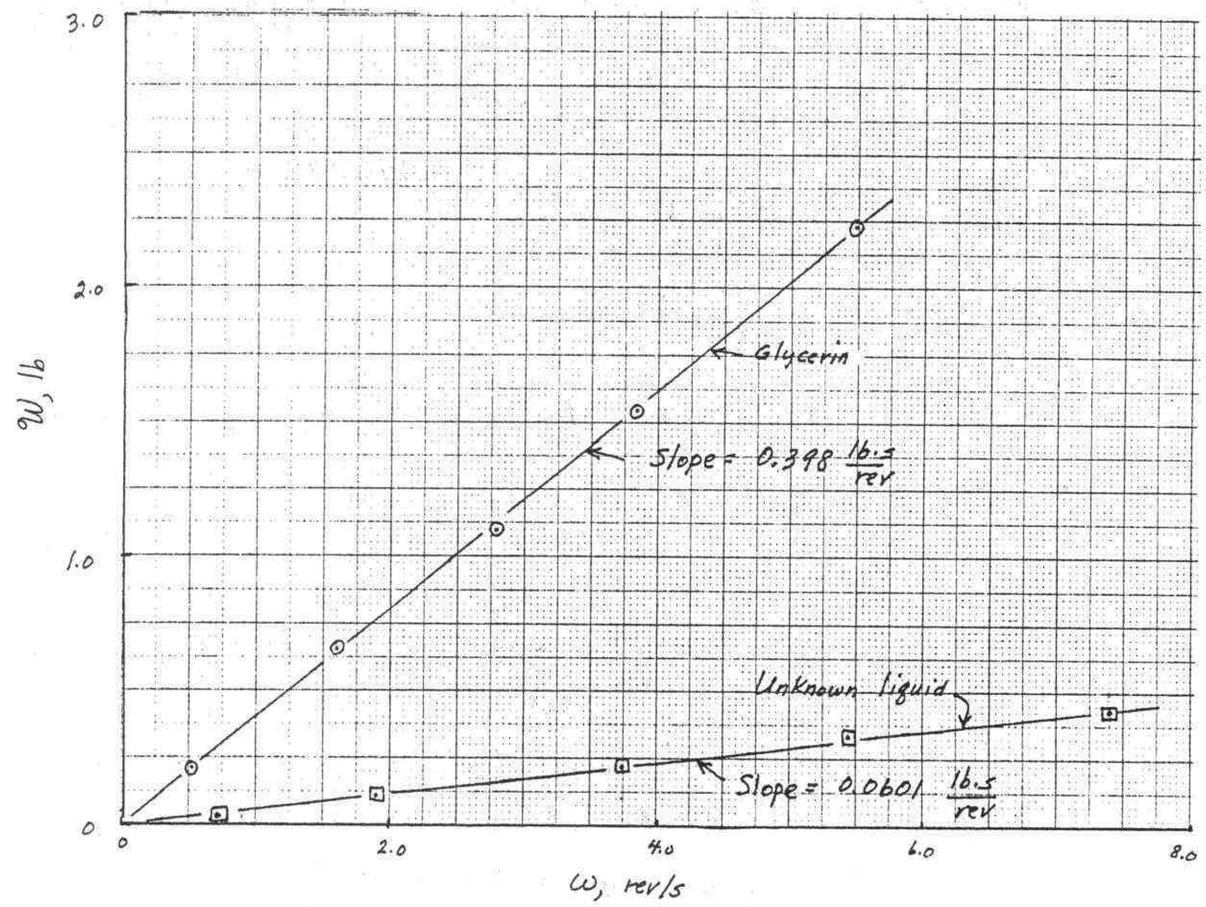
$$\text{slope (unknown fluid)} = 0.0601\ \frac{lb\cdot s}{rev}$$

(con't)

1.88 (con't)

Thus, from Eq.(1)

$$\mu\,(\text{unknown fluid}) = \frac{\text{slope}}{K} = \frac{0.0601\ \frac{lb\cdot s}{rev}}{12.7\ \frac{ft^2}{rev}} = \underline{\underline{4.73\times10^{-3}\ \frac{lb\cdot s}{ft^2}}}$$



1.89

1.89 A 12-in.-diameter circular plate is placed over a fixed bottom plate with a 0.1-in. gap between the two plates filled with glycerin as shown in Fig. P1.89. Determine the torque required to rotate the circular plate slowly at 2 rpm. Assume that the velocity distribution in the gap is linear and that the shear stress on the edge of the rotating plate is negligible.

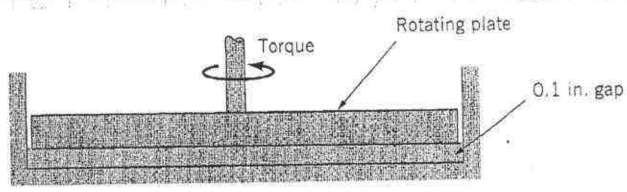


FIGURE P1.89

Torque, $d\mathcal{T}$, due to shearing stresses on plate is equal to

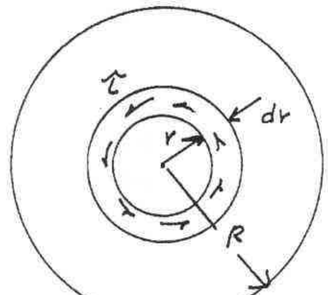
$$d\mathcal{T} = r\,\tau\,dA$$

where $dA = 2\pi r\,dr$. Thus,

$$d\mathcal{T} = r\,\tau\,2\pi r\,dr$$

and

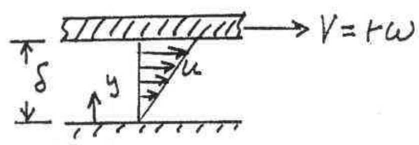
$$\mathcal{T} = 2\pi \int_0^R r^2 \tau\,dr$$



stresses acting on bottom of plate

Since $\tau = \mu \frac{du}{dy}$, and for a linear velocity distribution (see figure)

$$\tau = \mu \frac{r\omega}{\delta}$$



$$\frac{du}{dy} = \frac{V}{\delta} = \frac{r\omega}{\delta}$$

velocity distribution

Thus,

$$\mathcal{T} = \frac{2\pi\mu\omega}{\delta}\int_0^R r^3\,dr = \frac{2\pi\mu\omega}{\delta}\left(\frac{R^4}{4}\right)$$

and with the data given

$$\mathcal{T} = \frac{2\pi\left(0.0313\ \frac{lb\cdot s}{ft^2}\right)\left(2\ \frac{rev}{min}\right)\left(2\pi\ \frac{rad}{rev}\right)\left(\frac{1\ min}{60\ s}\right)\left(\frac{6}{12}\ ft\right)^4}{\left(\frac{0.1}{12}\ ft\right)(4)}$$

$$= \underline{0.0772\ ft\cdot lb}$$

1.91

1.91 Some measurements on a blood sample at 37 °C (98.6 °F) indicate a shearing stress of 0.52 N/m^2 for a corresponding rate of shearing strain of 200 s^{-1}. Determine the apparent viscosity of the blood and compare it with the viscosity of water at the same temperature.

$$\tau = \mu \frac{du}{dy} = \mu \dot{\gamma}$$

$$\mu_{blood} = \frac{\tau}{\dot{\gamma}} = \frac{0.52 \frac{N}{m^2}}{200 \frac{1}{s}} = \underline{\underline{26.0 \times 10^{-4} \frac{N \cdot s}{m^2}}}$$

From Table B.2 in Appendix B:

@ 30°C $\mu_{H_2O} = 7.975 \times 10^{-4} \frac{N \cdot s}{m^2}$

@ 40°C $\mu_{H_2O} = 6.529 \times 10^{-4} \frac{N \cdot s}{m^2}$

Thus, with linear interpolation, $\mu_{H_2O}(37°C) = 6.96 \times 10^{-4} \frac{N \cdot s}{m^2}$

and

$$\frac{\mu_{blood}}{\mu_{H_2O}} = \frac{26.0 \times 10^{-4} \frac{N \cdot s}{m^2}}{6.96 \times 10^{-4} \frac{N \cdot s}{m^2}} = \underline{\underline{3.74}}$$

1.93

1.93 A sound wave is observed to travel through a liquid with a speed of 1500 m/s. The specific gravity of the liquid is 1.5. Determine the bulk modulus for this fluid.

$c = \sqrt{\frac{E_v}{\rho}}$, where $\rho = SG\,\rho_{H_2O}$ and $SG = 1.5$

Thus,

$$E_v = c^2 \rho = c^2\, SG\, \rho_{H_2O}$$

$$= \left(1500 \frac{m}{s}\right)^2 (1.5)\left(999 \frac{kg}{m^3}\right)$$

$$= 3.37 \times 10^9 \frac{kg \cdot m}{s^2\, m^2}$$

or

$$E_v = 3.37 \times 10^9 \frac{N}{m^2}$$

59 bi

1.94

1.94 A rigid-walled cubical container is completely filled with water at 40 °F and sealed. The water is then heated to 100 °F. Determine the pressure that develops in the container when the water reaches this higher temperature. Assume that the volume of the container remains constant and the value of the bulk modulus of the water remains constant and equal to 300,000 psi.

Since the water mass remains constant,

$$\rho_{40^\circ} \forall = \rho_{100^\circ} (\forall + \Delta\forall)$$

where $\forall$ is volume and $\Delta\forall$ is change in volume if water were unconstrained during heating. Thus,

$$\frac{\Delta\forall}{\forall} = \frac{\rho_{40^\circ}}{\rho_{100^\circ}} - 1$$

From Table B.1 in Appendix B, $\rho_{40^\circ} = 1.940 \frac{slugs}{ft^3}$ and $\rho_{100^\circ} = 1.927 \frac{slugs}{ft^3}$

So that

$$\frac{\Delta\forall}{\forall} = \frac{1.940 \frac{slugs}{ft^3}}{1.927 \frac{slugs}{ft^3}} - 1 = 0.00675$$

From Eq. 1.12

$$E_v = -\frac{dp}{\frac{d\forall}{\forall}}$$

it follows with $d\forall \approx \Delta\forall$ and $dp \approx \Delta p$ that the change in pressure required to compress the water back to its original volume is

$$\Delta p = -(300{,}000 \text{ psi})(-0.00675)$$
$$= \underline{\underline{2.03 \times 10^3 \text{ psi}}}$$

1.95

1.95 In a test to determine the bulk modulus of a liquid it was found that as the absolute pressure was changed from 15 to 3000 psi the volume decreased from 10.240 to 10.138 in.³ Determine the bulk modulus for this liquid.

$$E_V = -\frac{dp}{d\forall/\forall} \qquad \text{(Eq. 1.12)}$$

Since

$$dp \approx \Delta p = 3000 - 15 = 2985 \text{ psi}$$

and

$$d\forall \approx \Delta\forall = 10.240 - 10.138 = 0.102 \text{ in.}^3$$

$$E_V \approx -\frac{2985 \frac{\text{lb}}{\text{in.}^2}}{\left(\frac{0.102 \text{ in.}^3}{10.240 \text{ in.}^3}\right)} = \underline{\underline{3.00 \times 10^5 \text{ psi}}}$$

1.96

1.96 Estimate the increase in pressure (in psi) required to decrease a unit volume of mercury by 0.1%.

$$E_v = -\frac{dp}{d\forall/\forall} \qquad (Eq. 1.12)$$

Thus,

$$\Delta p \approx -\frac{E_v \Delta\forall}{\forall} = -\left(4.14 \times 10^6 \frac{lb}{in.^2}\right)(-0.001)$$

$$\Delta p \approx \underline{\underline{4.14 \times 10^3 \ psi}}$$

1.97

1.97 A 1-m^3 volume of water is contained in a rigid container. Estimate the change in the volume of the water when a piston applies a pressure of 35 MPa.

$$E_v = -\frac{dp}{d\forall/\forall} \qquad (Eq. 1.12)$$

Thus,

$$\Delta\forall \approx -\frac{\forall \Delta p}{E_v} = -\frac{(1 \ m^3)(35 \times 10^6 \frac{N}{m^2})}{2.15 \times 10^9 \frac{N}{m^2}} = -0.0163 \ m^3$$

or

<u>decrease</u> in volume $\approx \underline{\underline{0.0163 \ m^3}}$

1.98

1.98 Determine the speed of sound at 20 °C in **(a)** air, **(b)** helium, and **(c)** natural gas. Express your answer in m/s.

$$c = \sqrt{kRT} \qquad (Eq.\ 1.20)$$

With $T = 20°C + 273 = 293\,K$:

(a) For air, $c = \sqrt{(1.40)\left(286.9\ \frac{J}{kg \cdot K}\right)(293K)} = \underline{\underline{343\ \frac{m}{s}}}$

(b) For helium, $c = \sqrt{(1.66)\left(2077\ \frac{J}{kg \cdot K}\right)(293\,K)} = \underline{\underline{1010\ \frac{m}{s}}}$

(c) For natural gas, $c = \sqrt{(1.31)\left(518.3\ \frac{J}{kg \cdot K}\right)(293K)} = \underline{\underline{446\ \frac{m}{s}}}$

1.99

1.99 Calculate the speed of sound in m/s for **(a)** gasoline, **(b)** mercury, and **(c)** seawater.

$$c = \sqrt{\frac{E_v}{\rho}} \qquad \text{(Eq. 1.19)}$$

(a) For gasoline: $c = \sqrt{\dfrac{1.3 \times 10^9 \frac{N}{m^2}}{680 \frac{kg}{m^3}}} = \underline{\underline{1.38 \frac{km}{s}}}$

(b) For mercury: $c = \sqrt{\dfrac{2.85 \times 10^{10} \frac{N}{m^2}}{1.36 \times 10^4 \frac{kg}{m^3}}} = \underline{\underline{1.45 \frac{km}{s}}}$

(c) For seawater: $c = \sqrt{\dfrac{2.34 \times 10^9 \frac{N}{m^2}}{1.03 \times 10^3 \frac{kg}{m^3}}} = \underline{\underline{1.51 \frac{km}{s}}}$

1.70

1.100

1.100 Air is enclosed by a rigid cylinder containing a piston. A pressure gage attached to the cylinder indicates an initial reading of 25 psi. Determine the reading on the gage when the piston has compressed the air to one-third its original volume. Assume the compression process to be isothermal and the local atmospheric pressure to be 14.7 psi.

For isothermal compression, $\frac{p}{\rho} = \text{constant}$ so that

$$\frac{p_i}{\rho_i} = \frac{p_f}{\rho_f}$$ where $i \sim$ initial state and $f \sim$ final state.

Thus, $$p_f = \frac{\rho_f}{\rho_i} p_i$$

Since $\rho = \frac{\text{mass}}{\text{volume}}$, $\frac{\rho_f}{\rho_i} = \frac{\text{initial volume}}{\text{final volume}} = 3$ (for constant mass)

and therefore

$$p_f = (3)\left[(25 + 14.7)\ \text{psi (abs)}\right] = 119\ \text{psi (abs)}$$

or

$$p_f\ (\text{gage}) = (119 - 14.7)\ \text{psi} = \underline{\underline{104\ \text{psi (gage)}}}$$

1.101

1.101 Repeat Problem 1.100 if the compression process takes place without friction and without heat transfer (isentropic process).

For isentropic compression, $\frac{p}{\rho^k}$ = constant so that

$$\frac{p_i}{\rho_i^k} = \frac{p_f}{\rho_f^k}$$ where $i \sim$ initial state and $f \sim$ final state.

Thus,

$$p_f = \left(\frac{\rho_f}{\rho_i}\right)^k p_i$$

Since $\rho = \frac{\text{mass}}{\text{volume}}$, $\frac{\rho_f}{\rho_i} = \frac{\text{initial volume}}{\text{final volume}} = 3$ (for constant mass)

and therefore

$$p_f = (3)^{1.40}\left[(25 + 14.7)\ \text{psi (abs)}\right] = 184.8\ \text{psi (abs)}$$

or

$$p_f\ (\text{gage}) = 184.8 - 14.7 = \underline{\underline{170\ \text{psi (gage)}}}$$

1.102

1.102 Carbon dioxide at 30 °C and 300 kPa absolute pressure expands isothermally to an absolute pressure of 165 kPa. Determine the final density of the gas.

For isothermal expansion, $\frac{p}{\rho}$ = constant so that

$$\frac{p_i}{\rho_i} = \frac{p_f}{\rho_f}$$ where $i \sim$ initial state and $f \sim$ final state.

Thus,

$$\rho_f = \frac{p_f}{p_i}\,\rho_i$$

Also,

$$\rho_i = \frac{p_i}{RT_i} = \frac{300 \times 10^3 \frac{N}{m^2}}{\left(188.9 \frac{J}{kg \cdot K}\right)\left[(30°C + 273)K\right]} = 5.24 \frac{kg}{m^3}$$

so that

$$\rho_f = \left(\frac{165\ kPa}{300\ kPa}\right)\left(5.24 \frac{kg}{m^3}\right) = \underline{\underline{2.88 \frac{kg}{m^3}}}$$

1.103

1.103 Oxygen at 30 °C and 300 kPa absolute pressure expands isothermally to an absolute pressure of 120 kPa. Determine the final density of the gas.

For isothermal expansion, $\frac{p}{\rho} = \text{constant}$ so that

$$\frac{p_i}{\rho_i} = \frac{p_f}{\rho_f}$$ where $i \sim$ initial state and $f \sim$ final state.

Thus,

$$\rho_f = \frac{p_f}{p_i}\rho_i$$

Also,

$$\rho_i = \frac{p_i}{RT_i} = \frac{300 \times 10^3 \frac{N}{m^2}}{\left(259.8 \frac{J}{kg \cdot K}\right)\left[(30°C + 273)K\right]} = 3.81 \frac{kg}{m^3}$$

so that

$$\rho_f = \left(\frac{120\ kPa}{300\ kPa}\right)\left(3.81 \frac{kg}{m^3}\right) = \underline{\underline{1.52 \frac{kg}{m^3}}}$$

1.73

1.104

1.104 Natural gas at 70 °F and standard atmospheric pressure of 14.7 psi (abs) is compressed isentropically to a new absolute pressure of 70 psi. Determine the final density and temperature of the gas.

For isentropic compression, $\frac{p}{\rho^k} = \text{constant}$ so that

$$\frac{p_i}{\rho_i^k} = \frac{p_f}{\rho_f^k}$$ where $i \sim$ initial state and $f \sim$ final state.

Thus,

$$\rho_f^k = \frac{p_f}{p_i}\rho_i^k$$

or

$$\rho_f = \left(\frac{p_f}{p_i}\right)^{\frac{1}{k}}\rho_i$$

Also,

$$\rho_i = \frac{p_i}{RT_i} = \frac{\left(14.7\,\frac{lb}{in.^2}\right)\left(144\,\frac{in.^2}{ft^2}\right)}{\left(3.099\times10^3\,\frac{ft\cdot lb}{slug\cdot{}^\circ R}\right)\left[(70^\circ F + 460)^\circ R\right]} = 1.29\times10^{-3}\,\frac{slugs}{ft^3}$$

so that

$$\rho_f = \left[\frac{70\text{ psi (abs)}}{14.7\text{ psi (abs)}}\right]^{\frac{1}{1.31}}\left(1.29\times10^{-3}\,\frac{slugs}{ft^3}\right) = \underline{\underline{4.25\times10^{-3}\,\frac{slugs}{ft^3}}}$$

and

$$T_f = \frac{p_f}{\rho_f R} = \frac{\left(70\,\frac{lb}{in.^2}\right)\left(144\,\frac{in.^2}{ft^2}\right)}{\left(4.25\times10^{-3}\,\frac{slugs}{ft^3}\right)\left(3.099\times10^3\,\frac{ft\cdot lb}{slug\cdot{}^\circ R}\right)}$$

$$= 765\ {}^\circ R$$

or

$$T_f = 765\,{}^\circ R - 460 = \underline{\underline{305\ {}^\circ F}}$$

1.105

1.105 Compare the isentropic bulk modulus of air at 101 kPa (abs) with that of water at the same pressure.

For air (Eq. 1.17),

$$E_v = kp = (1.40)(101 \times 10^3 \, Pa) = 1.41 \times 10^5 \, Pa$$

For water (Table 1.6)

$$E_v = 2.15 \times 10^9 \, Pa$$

Thus,

$$\frac{E_v \text{ (water)}}{E_v \text{ (air)}} = \frac{2.15 \times 10^9 \, Pa}{1.41 \times 10^5 \, Pa} = \underline{\underline{1.52 \times 10^4}}$$

1.75

*1.106

*1.106 Develop a computer program for calculating the final gage pressure of gas when the initial gage pressure, initial and final volumes, atmospheric pressure, and the type of process (isothermal or isentropic) are specified. Use BG units. Check your program against the results obtained for Problem 1.100.

1.70

For compression or expansion,

$$\frac{p}{\rho^k} = \text{constant}$$

where $k=1$ for isothermal process, and k = specific heat ratio for isentropic process. Thus,

$$\frac{p_i}{\rho_i^k} = \frac{p_f}{\rho_f^k}$$

where $i \sim$ initial state, $f \sim$ final state, so that

$$p_f = \left(\frac{\rho_f}{\rho_i}\right)^k p_i \qquad (1)$$

Since

$$\rho = \frac{\text{mass}}{\text{volume}}$$

then

$$\frac{\rho_f}{\rho_i} = \frac{V_i}{V_f}$$

where V_i, V_f, are the initial and final volumes, respectively. Thus, from Eq.(1)

$$p_{fg} + p_{atm} = \left(\frac{V_i}{V_f}\right)^k (p_{ig} + p_{atm}) \qquad (2)$$

where the subscript g refers to gage pressure. Equation (2) can be written as

$$p_{fg} = \left(\frac{V_i}{V_f}\right)^k (p_{ig} + p_{atm}) - p_{atm} \qquad (3)$$

A spreadsheet (EXCEL) program for calculating the final gage pressure follows.

(con't)

*1.106 (con't)

This program calculates the final gage pressure of an ideal gas when the initial gage pressure in psi, the initial volume, the final volume, the atmospheric pressure in psia, and the type of process (isothermal or isentropic) is specified. To use, replace current values and let k = 1 for isothermal process or k = specific heat for isentropic process.						
A	B	C	D	E	F	
Initial gage pressure	Initial volume	Final volume	Atmospheric pressure		Final gage pressure	
p_{ig}(psi)	V_i	V_f	p_{atm}(psia)	k	p_{fg}(psi)	
25	1	0.3333	14.7	1	104.4	Row 10

Formula:
=((B10/C10)^E10)*(A10+D10)-D10

Data from Problem 1.100 are included in the above table, giving a final gage pressure of 104.4 psi.

1.107

1.107 Often the assumption is made that the flow of a certain fluid can be considered as incompressible flow if the density of the fluid changes by less than 2%. If air is flowing through a tube such that the air pressure at one section is 9.0 psi and at a downstream section it is 8.6 psi at the same temperature, do you think that this flow could be considered an imcompressible flow? Support your answer with the necessary calculations. Assume standard atmospheric pressure.

For isothermal change in density

$$\frac{p_1}{\rho_1} = \frac{p_2}{\rho_2}$$

so that

$$\frac{\rho_2}{\rho_1} = \frac{p_2}{p_1}$$

The percent change in air densities between sections (1) & (2) is

$$\%\text{ change} = \frac{\rho_1 - \rho_2}{\rho_1} \times 100$$

$$= \left(1 - \frac{\rho_2}{\rho_1}\right) \times 100 = \left(1 - \frac{p_2}{p_1}\right) \times 100$$

Thus,

$$\%\text{ Change} = \left[1 - \frac{(8.6 + 14.7)\text{ psia}}{(9.0 + 14.7)\text{ psia}}\right] \times 100$$

$$= 1.69\%$$

Since $1.69\% < 2\%$ the flow could be considered incompressible.

Yes.

1.108

1.108 An important dimensionless parameter concerned with very high speed flow is the *Mach number*, defined as V/c, where V is the speed of the object such as an airplane or projectile, and c is the speed of sound in the fluid surrounding the object. For a projectile traveling at 800 mph through air at 50 °F and standard atmospheric pressure, what is the value of the Mach number?

$$\text{Mach number} = \frac{V}{c}$$

From Table B.3 in Appendix B

$$c_{air\,@\,50^\circ F} = 1106\ \frac{ft}{s}$$

Thus

$$\text{Mach number} = \frac{(800\ mph)\left(5280\ \frac{ft}{mi}\right)\left(\frac{1\ hr}{3600\ s}\right)}{1106\ \frac{ft}{s}}$$

$$= \underline{\underline{1.06}}$$

1.109

1.109 Jet airliners typically fly at altitudes between approximately 0 to 40,000 ft. Make use of the data in Appendix C to show on a graph how the speed of sound varies over this range.

$$c = \sqrt{kRT} \qquad \text{(Eq. 1.20)}$$

For $k = 1.40$ and $R = 1716 \frac{ft \cdot lb}{slug \cdot {}^\circ R}$

$$c = 49.0\sqrt{T({}^\circ R)}$$

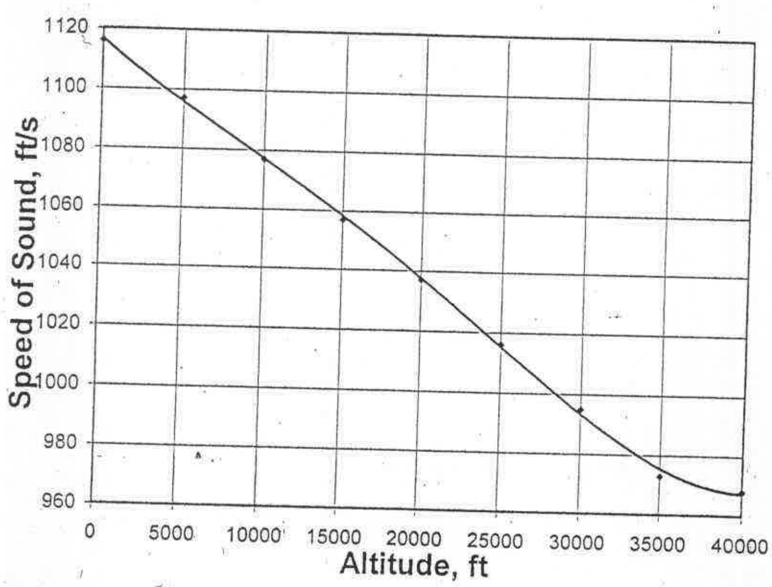
From Table C.1 in Appendix C at an altitude of 0 ft

$T = 59.00 + 460 = 519^\circ R$ so that

$$c = 49.0\sqrt{519^\circ R} = 1116 \frac{ft}{s}$$

Similar calculations can be made for other altitudes and the resulting graph is shown below.

Altitude, ft	Temp., °F	Temp., °R	c, ft/s
0	59	519	1116
5000	41.17	501.17	1097
10000	23.36	483.36	1077
15000	5.55	465.55	1057
20000	-12.26	447.74	1037
25000	-30.05	429.95	1016
30000	-47.83	412.17	995
35000	-65.61	394.39	973
40000	-69.7	390.3	968



1.110

1.110 (See Fluids in the News article titled "This water jet is a blast." Section 1.7.1) By what percent is the volume of water decreased if its pressure is increased to an equivalent to 3000 atmospheres (44,100 psi)?

$$E_v = -\frac{dp}{d\forall/\forall} \approx -\frac{\Delta p}{\Delta\forall/\forall} \qquad \text{(Eq. 1.12)}$$

$$\frac{\Delta\forall}{\forall} = -\frac{\Delta p}{E_v} = -\frac{44,100 \text{ psia} - 14.7 \text{ psia}}{3.12 \times 10^5 \text{ psia}} = -0.141$$

Thus,

% decrease in volume = $\underline{\underline{14.1\,\%}}$

1.111

1.111 During a mountain climbing trip it is observed that the water used to cook a meal boils at 90 °C rather than the standard 100 °C at sea level. At what altitude are the climbers preparing their meal? (See Tables B.2 and C.2 for data needed to solve this problem.)

When the water boils,

$p_{boil} = p_v$, where from Table B.2, at $T = 90°C$

$p_v = 7.01 \times 10^4 \frac{N}{m^2}$ (abs)

Also, from Table C.2, for a standard atmosphere

$p = 7.01 \times 10^4 \frac{N}{m^2}$ (abs) at an altitude of $\underline{\underline{3,000 \text{ m}}}$

65 bi

1.112

1.112 When a fluid flows through a sharp bend, low pressures may develop in localized regions of the bend. Estimate the minimum absolute pressure (in psi) that can develop without causing cavitation if the fluid is water at 160 °F.

Cavitation may occur when the local pressure equals the vapor pressure. For water at 160 °F (from Table B.1 in Appendix B)

$$p_v = 4.74 \text{ psi (abs)}$$

Thus, minimum pressure = $\underline{\underline{4.74 \text{ psi (abs)}}}$

1.113

1.113 A partially filled closed tank contains ethyl alcohol at 68 °F. If the air above the alcohol is evacuated what is the minimum absolute pressure that develops in the evacuated space?

Minimum pressure = vapor pressure = 0.85 psi (abs)

1.114

1.114 Estimate the minimum absolute pressure (in pascals) that can be developed at the inlet of a pump to avoid cavitation if the fluid is carbon tetrachloride at 20 °C.

Cavitation may occur when the suction pressure at the pump inlet equals the vapor pressure.

For carbon tetrachloride at 20°C $p_v = 13 \text{ kPa (abs)}$.

Thus, minimum pressure = $\underline{\underline{13 \text{ kPa (abs)}}}$

1.115

1.115 When water at 70 °C flows through a converging section of pipe, the pressure decreases in the direction of flow. Estimate the minimum absolute pressure that can develop without causing cavitation. Express your answer in both BG and SI units.

Cavitation may occur in the converging section of pipe when the pressure equals the vapor pressure. From Table B.2 in Appendix B for water at 70°C, $p_v = 31.2\ kPa\ (abs)$. Thus,

$$\text{minimum pressure} = \underline{\underline{31.2\ kPa\ (abs)}} \text{ in SI units.}$$

In BG units

$$\text{minimum pressure} = \left(31.2\times10^{3}\ \frac{N}{m^2}\right)\left(1.450\times10^{-4}\ \frac{psi}{\frac{N}{m^2}}\right)$$
$$= \underline{\underline{4.52\ psia}}$$

1.116.

1.116. At what atmospheric pressure will water boil at 35 °C? Express your answer in both SI and BG units.

The vapor pressure of water at 35°C is 5.81 kPa (abs) (from Table B.2 in Appendix B using linear interpolation). Thus, if water boils at this temperature the atmospheric pressure must be equal to $\underline{5.81\ kPa\ (abs)}$ in SI units. In BG units,

$$\left(5.81\times10^{3}\ \frac{N}{m^2}\right)\left(1.450\times10^{-4}\ \frac{\frac{N}{m^2}}{\frac{lb}{in^2}}\right) = \underline{\underline{0.842\ psi\ (abs)}}$$

1.118

1.118 When a 2-mm-diameter tube is inserted into a liquid in an open tank, the liquid is observed to rise 10 mm above the free surface of the liquid. the contact angle between the liquid and the tube is zero, and the specific weight of the liquid is 1.2×10^4 N/m^3. Determine the value of the surface tension for this liquid.

$$h = \frac{2\sigma \cos\theta}{\gamma R}, \quad \text{where } \theta = 0$$

Thus,

$$\sigma = \frac{\gamma h R}{2\cos\theta} = \frac{1.2\times10^{4}\,\frac{N}{m^3}\,(10\times10^{-3}\,m)(2\times10^{-3}\,m/2)}{2\cos 0}$$

$$= \underline{\underline{0.060\,\frac{N}{m}}}$$

1.119

1.119 An open 2-mm-diameter tube is inserted into a pan of ethyl alcohol and a similar 4-mm-diameter tube is inserted into a pan of water. In which tube will the height of the rise of the fluid column due to capillary action be the greatest? Assume the angle of contact is the same for both tubes.

$$h = \frac{2\sigma \cos\theta}{\gamma R} \qquad \text{(Eq. 1.22)}$$

Thus,

$$\frac{h\,(\text{alcohol})}{h\,(\text{water})} = \frac{\sigma(\text{alcohol})\,\gamma(\text{water})}{\sigma(\text{water})\,\gamma(\text{alcohol})}\left(\frac{4\text{ mm}}{2\text{ mm}}\right)$$

$$= \frac{\left(2.28\times10^{-2}\,\frac{N}{m}\right)\left(9.80\times10^{3}\,\frac{N}{m^3}\right)(4\text{ mm})}{\left(7.34\times10^{-2}\,\frac{N}{m}\right)\left(7.74\times10^{3}\,\frac{N}{m^3}\right)(2\text{ mm})}$$

$$= 0.787$$

Height of rise of water column is greatest.

1.120

1.120 Small droplets of carbon tetrachloride at 68 °F are formed with a spray nozzle. If the average diameter of the droplets is 200 μm what is the difference in pressure between the inside and outside of the droplets?

$$p = \frac{2\sigma}{R} \qquad \text{(Eq. 1.21)}$$

Since $\sigma = 2.69 \times 10^{-2} \frac{N}{m}$ at $68°F (= 20°C)$,

$$p = \frac{2\left(2.69 \times 10^{-2} \frac{N}{m}\right)}{100 \times 10^{-6} m} = \underline{\underline{538 \text{ Pa}}}$$

1.121

1.121 A 12-mm diameter jet of water discharges vertically into the atmosphere. Due to surface tension the pressure inside the jet will be slightly higher than the surrounding atmospheric pressure. Determine this difference in pressure.

For equilibrium (see figure),

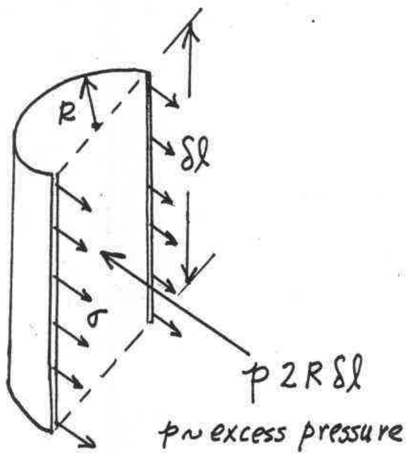
$$p(2R\delta l) = \sigma(2\delta l)$$

so that

$$p = \frac{\sigma}{R}$$

$$= \frac{7.34 \times 10^{-2}\ \frac{N}{m}}{\frac{12}{2} \times 10^{-3}\ m}$$

$$= \underline{\underline{12.2\ Pa}}$$



1.122

1.122 Estimate the excess pressure inside a rain drop having a diameter of 3 mm.

$$p = \frac{2\sigma}{R} \qquad \text{(Eq. 1.21)}$$

$$= \frac{2\,(7.34 \times 10^{-2}\ \frac{N}{m})}{0.0015\ m} = \underline{\underline{97.9\ Pa}}$$

1.23

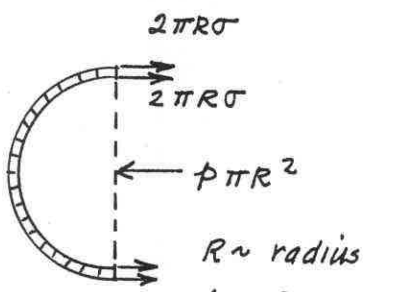
1.123 What is the difference between the pressure inside a soap bubble and atmospheric pressure for a 3-in.-diameter bubble? Assume the surface tension of the soap film to be 70% of that of water at 70 °F.

For equilibrium,

$$2(2\pi R\sigma) = p\pi R^2$$

or

$$p = \frac{4\sigma}{R}$$



(Note: There are two surfaces for bubble.)

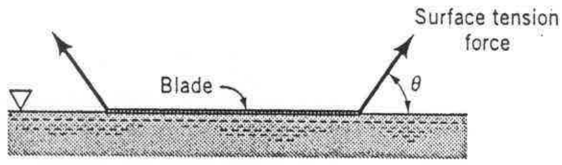
σ (water at 70°F) $= 4.97 \times 10^{-3} \frac{lb}{ft}$ (Table B.1 in Appendix B)

Thus,

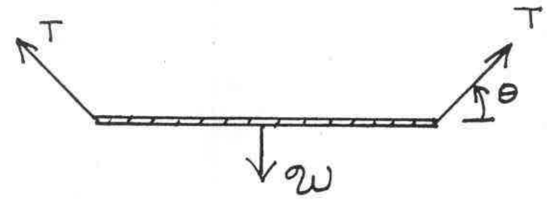
$$p = \frac{4(0.7)(4.97 \times 10^{-3} \frac{lb}{ft})}{\frac{1.5}{12} ft} = \underline{\underline{0.111 \frac{lb}{ft^2}}}$$

1.124

1.124 As shown in Video V1.9, surface tension forces can be strong enough to allow a double-edge steel razor blade to "float" on water, but a single-edge blade will sink. Assume that the surface tension forces act at an angle θ relative to the water surface as shown in Fig. P1.124. (a) The mass of the double-edge blade is 0.64×10^{-3} kg, and the total length of its sides is 206 mm. Determine the value of θ required to maintain equilibrium between the blade weight and the resultant surface tension force. (b) The mass of the single-edge blade is 2.61×10^{-3} kg, and the total length of its sides is 154 mm. Explain why this blade sinks. Support your answer with the necessary calculations.



■ FIGURE P1.124



(a) $\Sigma F_{vertical} = 0$

$$\mathcal{W} = T \sin\theta$$

where $\mathcal{W} = m_{blade} \times g$ and $T = \sigma \times$ length of sides.

$$\therefore \left(0.64 \times 10^{-3}\ kg\right)\left(9.81\ m/s^2\right) = \left(7.34 \times 10^{-2}\ \frac{N}{m}\right)\left(0.206\ m\right)\sin\theta$$

$$\sin\theta = 0.415$$

$$\underline{\underline{\theta = 24.5^\circ}}$$

(b) For single-edge blade

$$\mathcal{W} = m_{blade} \times g = \left(2.61 \times 10^{-3}\ kg\right)\left(9.81\ m/s^2\right)$$
$$= 0.0256\ N$$

and

$$T \sin\theta = \left(\sigma \times \text{length of blade}\right)\sin\theta$$
$$= \left(7.34 \times 10^{-2}\ N/m\right)\left(0.154\ m\right)\sin\theta$$
$$= 0.0113 \sin\theta$$

In order for blade to "float" $\mathcal{W} < T\sin\theta$. Since maximum value for $\sin\theta$ is 1, it follows that $\mathcal{W} > T\sin\theta$ and single-edge blade will sink.

1.125

1.125 To measure the water depth in a large open tank with opaque walls, an open vertical glass tube is attached to the side of the tank. The height of the water column in the tube is then used as a measure of the depth of water in the tank. **(a)** For a true water depth in the tank of 3 ft, make use of Eq. 1.22 (with $\theta \simeq 0°$) to determine the percent error due to capillarity as the diameter of the glass tube is changed. Assume a water temperature of 80 °F. Show your results on a graph of percent error versus tube diameter, D, in the range 0.1 in. $< D <$ 1.0 in. **(b)** If you want the error to be less than 1%, what is the smallest tube diameter allowed?

(a) The excess height, h, caused be the surface tension is

$$h = \frac{2\sigma \cos\theta}{\gamma R} \qquad \text{(Eq. 1.22)}$$

For $\theta \cong 0°$ with $D = 2R$

$$h = \frac{4\sigma}{\gamma D} \qquad (1)$$

From Table B.1 in Appendix B for water at 80°F $\sigma = 4.91 \times 10^{-3}$ lb/ft and $\gamma = 62.22$ lb/ft^3. Thus, from Eq. (1)

$$h(\text{ft}) = \frac{4\left(4.91 \times 10^{-3} \frac{\text{lb}}{\text{ft}}\right)}{\left(62.22 \frac{\text{lb}}{\text{ft}^3}\right) \frac{D(\text{in.})}{12 \text{ in./ft}}} = \frac{3.79 \times 10^{-3}}{D(\text{in.})} \qquad (2)$$

Since

$$\%\text{ error} = \frac{h(\text{ft})}{3 \text{ ft}} \times 100 \quad (\text{with the true depth} = 3 \text{ ft})$$

it follows from Eq. (2) that

$$\%\text{ error} = \frac{3.79 \times 10^{-3}}{3\,D(\text{in.})} \times 100$$

$$= \frac{0.126}{D(\text{in.})} \qquad (3)$$

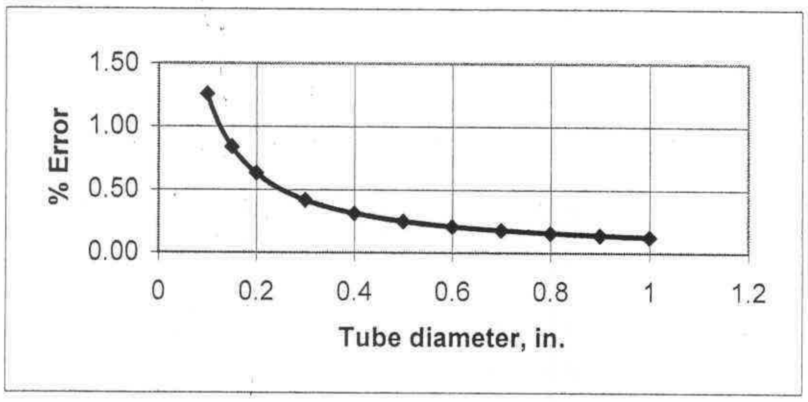
A plot of % error versus tube diameter is shown on the next page.

(con't)

1.125 (con't)

Diameter of tube, in.	% Error
0.1	1.26
0.15	0.84
0.2	0.63
0.3	0.42
0.4	0.32
0.5	0.25
0.6	0.21
0.7	0.18
0.8	0.16
0.9	0.14
1	0.13

Values obtained from Eq. (3)



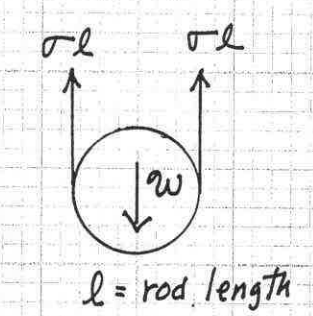
(b) For 1% error from Eq. (3)

$$1 = \frac{0.126}{D(in.)}$$

$$D = \underline{\underline{0.126 \text{ in.}}}$$

1.126

1.126 Under the right conditions, it is possible, due to surface tension, to have metal objects float on water. (See Video V1.9.) Consider placing a short length of a small diameter steel (sp. wt. = 490 lb/ft³) rod on a surface of water. What is the maximum diameter that the rod can have before it will sink? Assume that the surface tension forces act vertically upward. *Note:* A standard paper clip has a diameter of 0.036 in. Partially unfold a paper clip and see if you can get it to float on water. Do the results of this experiment support your analysis?



In order for rod to float (see figure) it follows that

$$2\sigma\ell \geq \mathcal{W} \geq \left(\frac{\pi}{4}\right)(D^2)\,\ell\,\gamma_{steel}$$

Thus, for the limiting case

$$D_{max}^2 = \frac{2\sigma\ell}{\left(\frac{\pi}{4}\right)\ell\,\gamma_{steel}} = \frac{8\sigma}{\pi\,\gamma_{steel}}$$

so that

$$D_{max} = \left[\frac{8\left(5.03\times10^{-3}\ \frac{lb}{ft}\right)}{\pi\left(490\ \frac{lb}{ft^3}\right)}\right]^{1/2} = 5.11\times10^{-3}\ ft$$

$$= \underline{\underline{0.0614\ in.}}$$

Since a standard steel paper clip has a diameter of 0.036 in., which is less than 0.0614 in., it should float. A simple experiment will verify this. <u>Yes</u>.

1.127

1.127 An open, clean glass tube, having a diameter of 3 mm, is inserted vertically into a dish of mercury at 20 °C. How far will the column of mercury in the tube be depressed?

$$h = \frac{2\sigma \cos\theta}{\gamma R} \qquad \text{(Eq. 1.22)}$$

For $\theta = 130°$,

$$h = \frac{2\left(4.66 \times 10^{-1} \frac{N}{m}\right) \cos 130°}{\left(133 \times 10^{3} \frac{N}{m^3}\right)(0.0015\ m)} = -3.00 \times 10^{-3}\ m$$

Thus, column will be depressed $\underline{\underline{3.00\ mm}}$

1.128

1.128 An open, clean glass tube ($\theta = 0°$) is inserted vertically into a pan of water. What tube diameter is needed if the water level in the tube is to rise one tube diameter (due to surface tension)?

$$h = \frac{2\sigma \cos\theta}{\gamma R} \qquad \text{(Eq. 1.22)}$$

For $h = 2R$ and $\theta = 0°$

$$2R = \frac{2\sigma(1)}{\gamma R}$$

and

$$R^2 = \frac{\sigma}{\gamma} = \frac{5.03 \times 10^{-3} \frac{lb}{ft}}{62.4 \frac{lb}{ft^3}}$$

$$R = 8.98 \times 10^{-3}\ ft$$

$$\text{diameter} = 2R = \underline{\underline{1.80 \times 10^{-2}\ ft}}$$

70 bi

1.129

1.129 Determine the height water at 60 °F will rise due to capillary action in a clean, $\frac{1}{4}$-in.-diameter tube. What will be the height if the diameter is reduced to 0.01 in.?

$$h = \frac{2\sigma\cos\theta}{\gamma R} \qquad \text{(Eq. 1.22)}$$

For water at 60°F (from Table B.1 in Appendix B),

$\sigma = 5.03 \times 10^{-3}\ \frac{lb}{ft}$ and $\gamma = 62.37\ \frac{lb}{ft^3}$. Thus, with $\theta = 0$,

(for $R = 0.125$ in.)

$$h = \frac{2\left(5.03\times10^{-3}\ \frac{lb}{ft}\right)(1)}{\left(62.37\ \frac{lb}{ft^3}\right)\left(\frac{0.125}{12}\ ft\right)} = 1.55\times10^{-2}\ ft$$

or

$$h = \left(1.55\times10^{-2}\ ft\right)\left(\frac{12\ in.}{ft}\right) = \underline{\underline{0.186\ in.}}$$

Similarly,

(for $R = 0.005$ in.)

$$h = (0.186\ in.)\left(\frac{0.125\ in.}{0.005\ in.}\right) = \underline{\underline{4.65\ in.}}$$

1.130

1.130 Two vertical, parallel, clean, glass plates are spaced a distance of 2 mm apart. If the plates are placed in water how high will the water rise between the plates due to capillary action?

For equilibrium in the vertical direction,

$$W = 2(\sigma \ell \cos\theta)$$

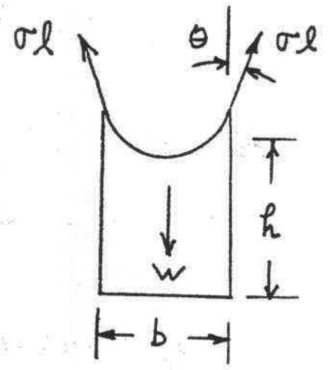
Since,

$$W = \gamma h b \ell$$

$$\gamma h b \ell = 2\sigma \ell \cos\theta$$

or,

$$h = \frac{2\sigma\cos\theta}{\gamma b}$$



($\ell \sim$ width of plates)

Thus, (for $\theta = 0$)

$$h = \frac{2\left(7.34\times10^{-2}\ \frac{N}{m}\right)(1)}{\left(9.80\times10^{3}\ \frac{N}{m^3}\right)(0.002\ m)} = 7.49\times10^{-3}\ m = \underline{\underline{7.49\ mm}}$$

1.131

1.131 (See Fluids in the News article titled "Walking on water," Section 1.9.) (**a**) The water strider bug shown in Fig. P1.131 is supported on the surface of a pond by surface tension acting along the interface between the water and the bug's legs. Determine the minimum length of this interface needed to support the bug. Assume the bug weighs 10^{-4} N and the surface tension force acts vertically upwards. (**b**) Repeat part (a) if surface tension were to support a person weighing 750 N.

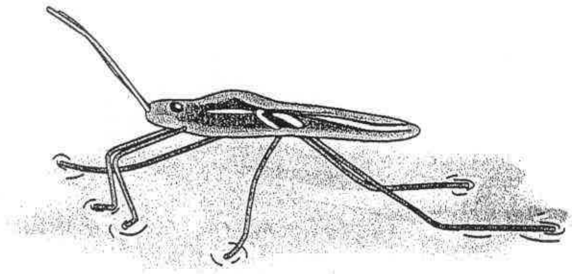
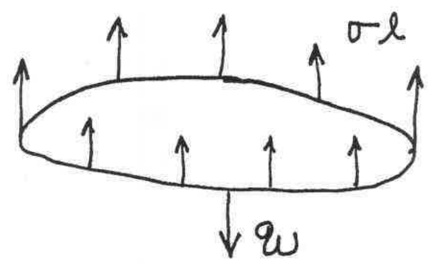


FIGURE P1.131

For equilibrium,

$$\mathcal{W} = \sigma \ell$$



$\mathcal{W} \sim$ weight
$\sigma \sim$ surface tension
$\ell \sim$ length of interface

(a)
$$\ell = \frac{\mathcal{W}}{\sigma} = \frac{10^{-4}\,N}{7.34 \times 10^{-2}\,\frac{N}{m}}$$
$$= 1.36 \times 10^{-3}\,m$$
$$= (1.36 \times 10^{-3}\,m)\left(10^{3}\,\frac{mm}{m}\right) = \underline{\underline{1.36\,mm}}$$

(b)
$$\ell = \frac{750\,N}{7.34 \times 10^{-2}\,\frac{N}{m}} = \underline{\underline{1.02 \times 10^{4}\,m}} \quad (6.34\,mi\,!!)$$

1.1LP

1.1LP Fluid Characterization by Use of a Stormer Viscometer

Objective: As discussed in Section 1.6, some fluids can be classified as Newtonian fluids; others are non-Newtonian. The purpose of this experiment is to determine the shearing stress versus rate of strain characteristics of various liquids and, thus, to classify them as Newtonian or non-Newtonian fluids.

Equipment: Stormer viscometer containing a stationary outer cylinder and a rotating, concentric inner cylinder (see Fig. P1.1LP); stop watch; drive weights for the viscometer; three different liquids (silicone oil, Latex paint, and corn syrup).

Experimental Procedure: Fill the gap between the inner and outer cylinders with one of the three fluids to be tested. Select an appropriate drive weight (of mass m) and attach it to the end of the cord that wraps around the drum to which the inner cylinder is fastened. Release the brake mechanism to allow the inner cylinder to start to rotate. (The outer cylinder remains stationary.) After the cylinder has reached its steady-state angular velocity, measure the amount of time, t, that it takes the inner cylinder to rotate N revolutions. Repeat the measurements using various drive weights. Repeat the entire procedure for the other fluids to be tested.

Calculations: For each of the three fluids tested, convert the mass, m, of the drive weight to its weight, $W = mg$, where g is the acceleration of gravity. Also determine the angular velocity of the inner cylinder, $\omega = N/t$.

Graph: For each fluid tested, plot the drive weight, W, as ordinates and angular velocity, ω, as abscissas. Draw a best fit curve through the data.

Results: Note that for the flow geometry of this experiment, the weight, W, is proportional to the shearing stress, τ, on the inner cylinder. This is true because with constant angular velocity, the torque produced by the viscous shear stress on the cylinder is equal to the torque produced by the weight (weight times the appropriate moment arm). Also, the angular velocity, ω, is proportional to the rate of strain, du/dy. This is true because the velocity gradient in the fluid is proportional to the inner cylinder surface speed (which is proportional to its angular velocity) divided by the width of the gap between the cylinders. Based on your graphs, classify each of the three fluids as to whether they are Newtonian, shear thickening, or shear thinning (see Fig. 1.7).

Data: To proceed, print this page for reference when you work the problem and *click here* to bring up an EXCEL page with the data for this problem.

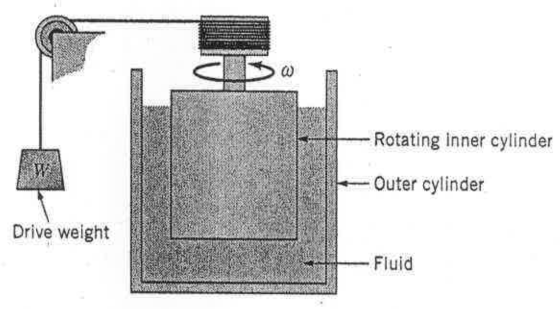


FIGURE P1.1LP

(con't)

1.1LP (con't)

Solution for Problem 1.1LP Fluid Characterization by Use of a Stormer Viscometer

m, kg	N, revs	t, s	ω, rev/s	W, N
Silicone Oil Data				
0.02	4	59.3	0.07	0.20
0.05	12	66.0	0.18	0.49
0.10	24	64.2	0.37	0.98
0.15	20	35.0	0.57	1.47
0.20	24	31.7	0.76	1.96
0.25	30	31.0	0.97	2.45
0.30	20	17.4	1.15	2.94
0.35	25	18.8	1.33	3.43
0.40	40	26.0	1.54	3.92
Corn Syrup Data				
0.05	1	28.2	0.04	0.49
0.10	2	27.5	0.07	0.98
0.20	4	27.2	0.15	1.96
0.40	8	25.7	0.31	3.92
Latex Paint Data				
0.02	2	32.7	0.06	0.20
0.03	2	20.2	0.10	0.29
0.04	5	32.2	0.16	0.39
0.05	10	47.3	0.21	0.49
0.06	10	37.2	0.27	0.59
0.07	10	29.8	0.34	0.69
0.08	10	24.6	0.41	0.78
0.09	10	20.1	0.50	0.88
0.10	20	34.0	0.59	0.98

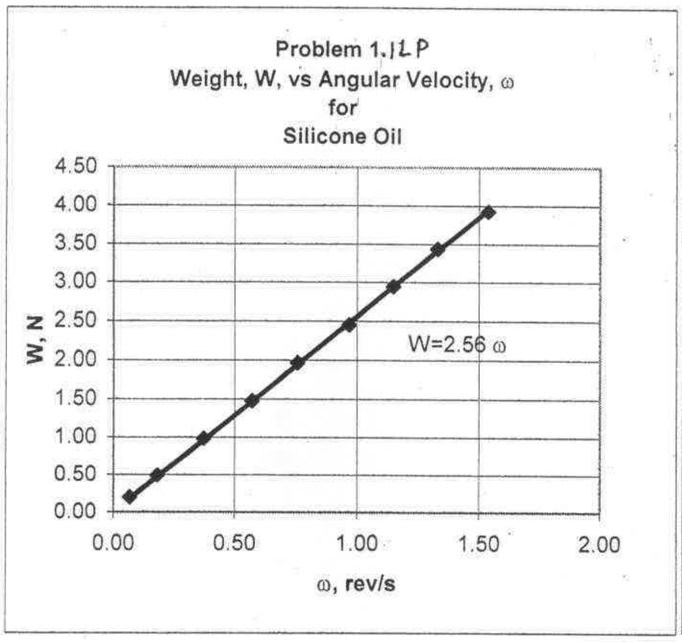
From the graphs:
Silicone oil is Newtonian
Corn Syrup is Newtonian
Latex paint is shear thinning

$\omega = N/t$

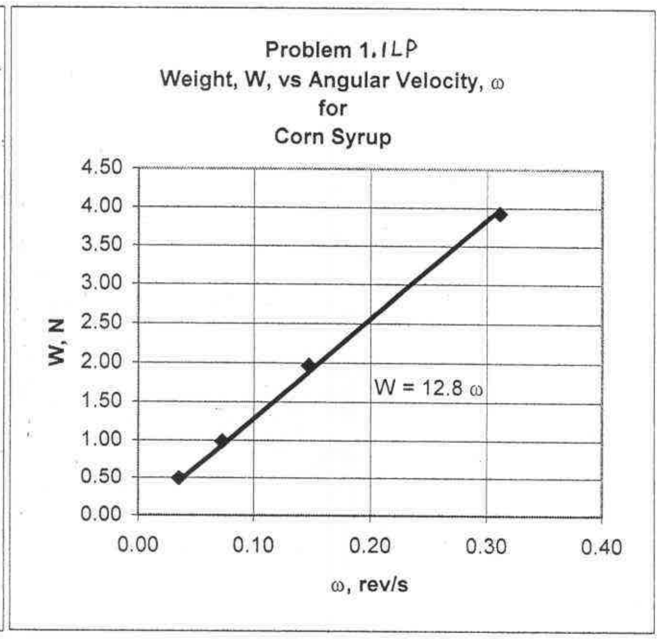
$W = mg$

(con't)

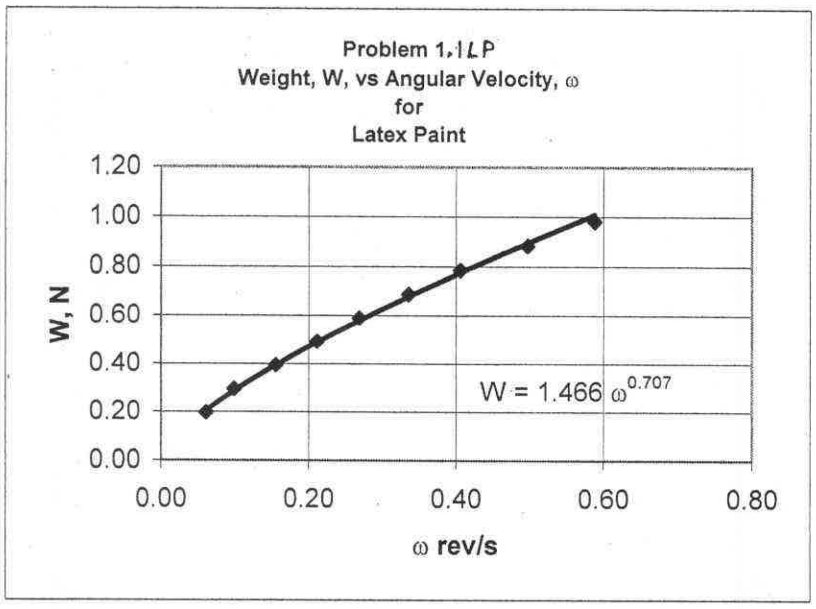
1.1LP (Con't)



Problem 1.1LP
Weight, W, vs Angular Velocity, ω
for
Silicone Oil
W, N
ω, rev/s
W=2.56 ω



Problem 1.1LP
Weight, W, vs Angular Velocity, ω
for
Corn Syrup
W, N
ω, rev/s
W = 12.8 ω



Problem 1.1LP
Weight, W, vs Angular Velocity, ω
for
Latex Paint
W, N
ω rev/s
W = 1.466 ω0.707

1.2LP

1.2LP Capillary Tube Viscometer

Objective: The flowrate of a viscous fluid through a small diameter (capillary) tube is a function of the viscosity of the fluid. For the flow geometry shown in Fig. P1.2LP the kinematic viscosity, ν, is inversely proportional to the flowrate, Q. That is, $\nu = K/Q$, where K is the calibration constant for the particular device. The purpose of this experiment is to determine the value of K and to use it to determine the kinematic viscosity of water as a function of temperature.

Equipment: Constant temperature water tank, capillary tube, thermometer, stop watch, graduated cylinder.

Experimental Procedure: Adjust the water temperature to 15.6°C and determine the flowrate through the capillary tube by measuring the time, t, it takes to collect a volume, V, of water in a small graduated cylinder. Repeat the measurements for various water temperatures, T. Be sure that the water depth, h, in the tank is the same for each trial. Since the flowrate is a function of the depth (as well as viscosity), the value of K obtained will be valid for only that value of h.

Calculations: For each temperature tested, determine the flowrate, $Q = V/t$. Use the data for the 15.6°C water to determine the calibration constant, K, for this device. That is, $K = \nu Q$, where the kinematic viscosity for 15.6°C water is given in Table 1.5 and Q is the measured flowrate at this temperature. Use this value of K and your other data to determine the viscosity of water as a function of temperature.

Graph: Plot the experimentally determined kinematic viscosity, ν, as ordinates and temperature, T, as abscissas.

Results: On the same graph, plot the standard viscosity-temperature data obtained from Table B.2.

Data: To proceed, print this page for reference when you work the problem and *click here* to bring up an EXCEL page with the data for this problem.

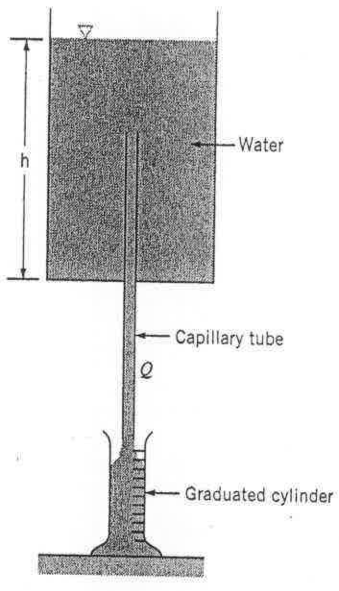


FIGURE P1.2LP

(con't)

1.2LP (Con't)

Solution for Problem 1.2LP Capillary Tube Viscometer

V, ml	t, s	T, deg C	Q, ml/s	ν, m^2/s
9.2	19.8	15.6	0.465	1.12E-06
9.7	15.8	26.3	0.614	8.49E-07
9.2	16.8	21.3	0.548	9.51E-07
9.1	21.3	12.3	0.427	1.22E-06
9.2	13.1	34.3	0.702	7.42E-07
9.4	10.1	50.4	0.931	5.60E-07
9.1	8.9	58.1	1.022	5.10E-07

From Table B.2

T, deg C	ν, m^2/s
10	1.31E-06
20	1.00E-06
30	8.01E-07
40	6.58E-07
50	5.53E-07
60	4.75E-07

ν = K/Q   K, m^2 ml/s^2: 5.21E-07   ν (at 15.6 deg C), m^2/s: 1.12E-06

K = ν Q = 1.12E-6 m^2/s * 0.465 ml/s = 5.21E-7 m^2 ml/s^2